# **RKI** Exploration & Production LLC

210 Park Avenue, Suite 900, Oklahoma City, OK 73102 405-949-2221 Fax 405-949-2223

July 17, 2015

Cole Anderson NSR Program Manager Department of Environmental Quality, Air Quality Division Herschler Building, 2-E 122 West 25th Street Cheyenne, WY 82002 JUL 21 2015

AIR QUALITY DIVISION

Re:

Air Permit Application

RKI Exploration & Production LLC

Split Hill Unit 37-68-27 PAD (1TH & 3TH) (API#: 49-009-30065 & 49-009-30064)

Dear Mr. Anderson:

Pursuant to the requirements of the Wyoming Air Quality Standards and Regulations New Source Review permitting program and the associated Chapter 6 Section 2 (C6 S2) Oil and Gas Production Facilities Permitting Guidance document dated September 2013, RKI Exploration & Production LLC (RKI) submits this *C6 S2 Application for an Air Quality Permit* for the subject wellpad.

Split Hill Unit 37-68-27 1TH is an oil well situated in Converse County. First day of production (FDOP) was April 28, 2015.

Split Hill Unit 37-68-27 3TH is an oil well situated in Converse County. First day of production (FDOP) was April 28, 2015.

The site consists of two oil wells, oil and produced water storage tanks, two 2-phase separators (unfired), two heater-treaters, a combination high pressure/low pressure flare used to combust gas flashed from the storage tanks, load out facilities and heater treaters . Gas is currently being flared. Produced liquids are loaded out by truck.

Average daily production for the <u>pad</u>, 30 days after FDOP, was 169-bbl oil, 93-mcf gas, and 317-bbl water.

Please direct any concerns with the information contained in this application to me at the phone number or email address listed in the application.

Sincerely,

Jeffrey L. Ingerson

Senior Air Permitting Engineer

Reviewer <u>HmB</u>
cc:
Modeler \_\_\_\_
D.E. \_\_\_
File \_\_A001351

# DE PARAMONTO ENVIRONMENTAL OF THE PARAMONTO OF THE PARAMO

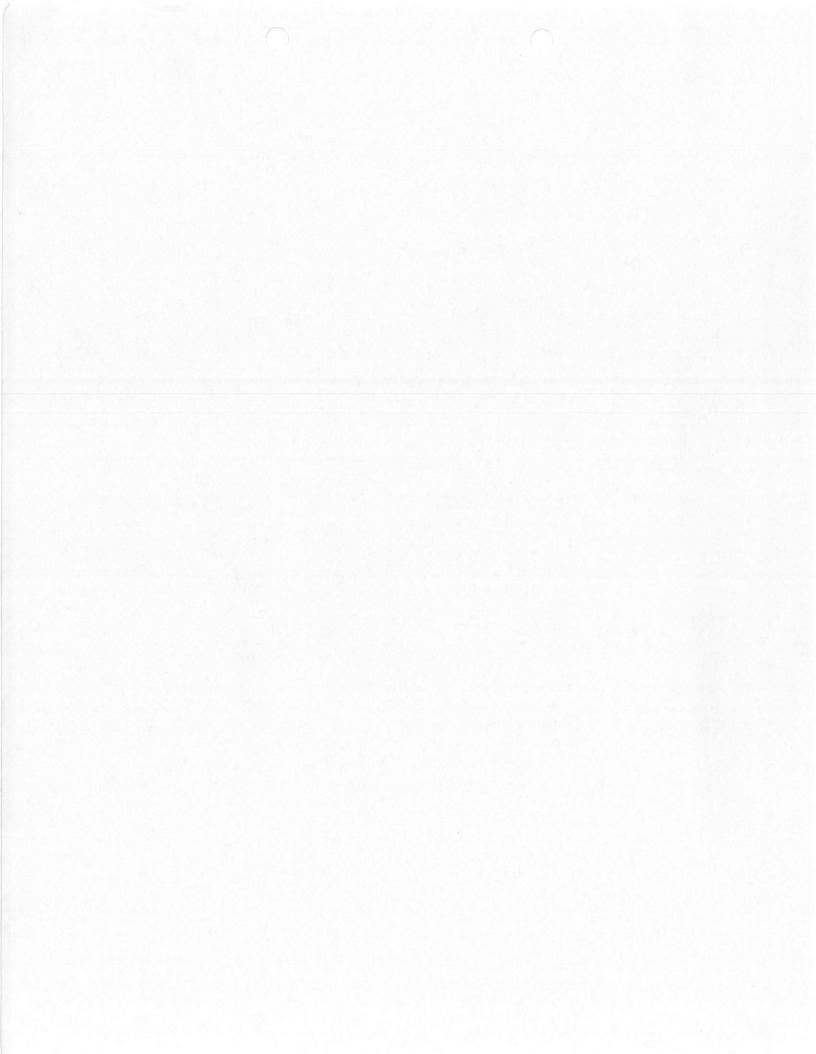
#### **Department of Environmental Quality Air Quality Division**

## Permit Application Form

WYOMING		Is this a revision t	to an existing a	application	1?				
		Yes	Yes No X			Date of Application:			7/17/2015
		Previous Applicat	tion #:						
COMPA	NY INFOR	RMATION:							
Company I				RKI Explo	oration & P	roduction, LLC			
Address:			210 Pa		e, Suite 90				
City:	Oklahor	na City	State:	Oklaho				Zip Code:	73102
Country:		USA	]	Phone	Number:		(405) 949-		
(-0.00 -0.00 0.00 0.00 0.00 0.00 0.00 0.	INFORM	ATION:	-		•				-
Facility Na				Sp	lit Hill Unit	27 PAD			
-	ty or Existin	g Facility:	New						
Facility Des	10-V 2011 2015 10-0-2015	8		Oil Pr	oduction W	/ellsite/Pad			
Facility Cla	-	Minor	T T		ng Status:		perating	T	
Facility Typ			uction Site				,		
7 - 71									
For Oil & G	as Product	ion Sites ONLY:							
First Date	of Productio	on (FDOP)/Date of	f Modification	:		4/28/2015			
Does produ	uction at th	is facility contain	H2S?*		No				
*If yes, cor	ntact the Di	vision.							
API Numbe			Sp	lit Hill Uni	t 37-69-36	1TH (API # 49	-009-30065	)	
			Sp	lit Hill Uni	t 37-69-36	3TH (API # 49	-009-30064	)	
NAICS Cod	e:		211	111 Crude	Petroleum	and Natural (	Sas Extracti	on	
FACILITY	LOCATION	ON:							
		 on in either the latitu	ude/longitude a	rea or section	on/township	/range area. Bo	th are not re	auired.	
Physical Ad			,		,	,		,	
City:			Zip	Code:					
State:	WY		County:	Conve	rse				
OR									
Latitude:	43.14	1725	ongitude:	-105.01	626				
Quarter Qu				Quarter:	1020				
Section:	27	SW SW	_ Township:	37N	I			Range:	68W
		and latitude, use	DEPO-DE INCOCUENTATION OF THE			s after the dea	rimal (i e 4	_	
			1470 037 11 03	o- autum	una 5 aigit	s after the act	innai (i.c. 4	1.12545, -10	7.50765)
		MATION:					•		
		AND NSR Permitting Co		or your applica	ation to be dee		he agency.		
Title:	Mr.		irst Name:			Jeffrey			
Last Name		In	gerson	DIU E					
Company i	Name:		<u> </u>			roduction, LLC			
Job Title:					ermitting E			-	
Address:		ahama Cita			eneue, Su			Т	
City:	Okl	ahoma City	- Sta	ite:		Oklaho	ma		
Zip Code:	Dhana N-	73102			F 21			a Malaiser	
	Phone No.: Phone No.:	(405) 987-2			E-mail:			@rkixp.com	
		(405) 820-1		,	Fax No.:			949-2223	
Contact Ty	pe:	NSR Permitting	Contact	2	Start Date:		iviar	ch, 2014	

Additional Contact <sup>-</sup>	Type (if needed):									
Title: Mr.	1r. First Name: Charles									
Last Name:	Ahn									
Company Name:		RKI Exploration & F	Production, LLC							
Job Title:	***************************************	Manager, EHS/Regul								
Address:		10 Park Aveneue, Su								
City: O	klahoma City Sta	homa City State: Oklahoma								
Zip Code:	73102									
Primary Phone No.:										
Mobile Phone No.:		Fax No.:	(405) 949-2	223						
Contact Type:	Compliance contact	Start Date:	March, 20	14						
FACILITY APPLI	CATION INFORMATION:	3								
General Info:										
The state of the s	nged location or is it a new/ green	field facility?	Ye	25						
	nning document been included in t		N							
	d in a sage grouse core area?*	ins application:	I N							
	sage grouse core area, what is the	WFR number?								
	ut sage grouse core area, contact		nartment							
			sartment.							
	Applicability - Facility Leve	<u>1:</u>								
977	ficant Deterioration (PSD):		N							
Non-Attainment Ne			N	0						
Modeling Secti										
	Division been contacted to detern	nine if modeling is re	quired?	0						
Is a modeling analys	sis part of this application?		N	0						
Is the proposed pro	ject subject to Prevention of Signi	ificant Deterioration (	(PSD) requirements?	0						
	Division been notified to schedule									
	tocol been submitted to and appr			0						
	Division received a Q/D analysis to									
the need for an AQI				О						
Required Attac										
Facility Map	<u>√</u>									
Process Flow Diagra										
Modeling Analysis (										
Land Use Planning [										
Detailed Project De	process,									
Emissions Calculation										
Emissions Calculation	5.13									
l,	Jeffrey L. Ingerson		Senior Air Permitting E	ingineer						
	Responsible Official (Printed	Name)	Title							
an Official Penreser	ntative of the Company state that	t I have knowledge of	the facts herein set forth and the	nat the same						

an Official Representative of the Company, state that I have knowledge of the facts herein set forth and that the same are true and correct to the best of my knowledge and belief. I further certify that the operational information provided and emission rates listed on this application reflect the anticipated emissions due to the operation of this facility. The facility will operate in compliance with all applicable Wyoming Air Quality Standards and Regulations.



## Separator/Treater

Company Equipment II	):	HTR01 1TH				
Company Equipment D	escription:	Horizontal Hea	eater Treater w/ 0.500 mmbtu burner			
Operating Status	Oneratina					
Operating Status:	Operating					
Initial Construction Cor		. / /	10045			
Initial Operation Comm	· · · · · · · · · · · · · · · · · · ·	4/28/	/2015			
Most Recent Construct	ion/ Modification					
Commencement Date:						
Select reason(s) for the		cluded in this applicati	tion (must be completed regardless of date			
of installation or modi		C: 11/01 = 11:. \	1			
Reason:	Construction (Green	field/New Facility)				
If reason is <i>Reconstruc</i> Type of Vessel:	tion or Temporary Permi	it or <i>Other,</i> please expl				
Operating Temperatur		100				
Operating Pressure (ps		85	-			
	ce Classification Code(s)	(SCC) that describe the	e process(es) performed by the emission			
		1-00-111-00				
Potential Operating So Hours/day: Hours/year		perating schedule for th  24  8760	this emission unit. –			

Control Equipment: Yes							
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.							
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?							
☐ Yes ☑ No							
Pollutant:							
Proposed BACT:							
*If yes, attach BACT Analysis with this application.							
Lowest Achievable Emission Pate (LAEP), Was a LAEP Analysis completed for this emission unit?							
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?  Ves  No							
Pollutant:							
Proposed LAER:							
*If yes, attach LAER Analysis with this application.							
n yes, accord a ten Analysis with this application.							
Federal and State Rule Applicability:							
New Source Performance Standards (NSPS): Not Effected							
New Source Performance Standard are listed under 40 CFR 60-							
Standards of Performance for New Stationary Sources.							
NSPS Subpart:							
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected							
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR							
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).							
Part 61 NESHAP Subpart:							
Motional Engineers Standards for Hannadaya Air Dellatarts (NECHAD Dart C2)							
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected  Not Effected							
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63							
Part 63 NESHAP Subpart:							
Prevention of Significant Deterioration (PSD): Not Affected							
These rules are found under WAQSR Chapter 6, Section 4.							
moss raise are really array tringert enaptor o, coolien 4.							
Non-Attainment New Source Review: Not Affected							
These rules are found under WAQSR Chapter 6, Section 13.							

HTR01 1TH

**Emissions Information-** The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

			Effic	ciency Standards			
		Pre-Controlled Potential Emissions	Potential to Emit		Potential to Emit	Potential to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
eria Po	llutants:						
1.)	Particulate emissions (PE/PM) (formerly particulate matter, PM)						
2.)	PM #10 microns in diameter (PE/PM10)	0.011			0.0026	0.011	AP-42
3.)	PM #2.5 microns in diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)	0.001			0.0002	0.001	AP-42
5.)	Nitrogen Oxides (NOx)	0.147			0.0336	0.147	AP-42
6.)	Carbon monoxide (CO)	0.123			0.0282	0.123	AP-42
7.)	Volatile organic compounds (VOC)	0.008			0.0018	0.008	AP-42
8.)	Lead (Pb)						
9.)	Total Hazrdous Air Pollutants (HAPs)	0.003			0.0006	0.003	AP-42
10.)	Fluoride (F)						
11.)	Hydrogen Sulfide (H2S)	0			0	0	AP-42
12.)	Mercury (Hg)						
13.)	Total Reduced Sulfur (TRS)						
14.)	Sulfuric Acid Mist (SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	Efficiency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	-					
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

				_		
		Effic	Efficiency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	-				***************************************	
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

## Storage Tank/Silo

Company Equipment ID	OILTNK 1-4 1TH							
Company Equipment De	escription:		4 x 400 bbl Oil Storage Tanks					
Operating Status:	Operating							
Initial Construction Con	nmencement Date:		T)					
<b>Initial Operation Comm</b>	encement Date:		4/28	/2015				
Most Recent Constructi	on/ Modification					-		
Commencement Date:								
Most Recent Operation	Commencement Date:							
Select reason(s) for this	s emissions unit being i	ncluded in t	his applicat	ion (must k	e complete	d regardless of date of		
installation or modifica	tion):							
Reason:	Construction (Gree	nfield/New	Facility)	_				
If reason is Reconstruct	<b>ion</b> or <b>Temporary Pern</b>	nit or Other,	please exp	lain below:				
_								
Material Type:	Liquid							
Description of Material	Stored:			Cru	de Oil			
Capacity:	400	_	Units:	barrels				
Maximum Throughput:		25915			Units:	barrels/yr		
Maximum Hourly Throu	ghput:	2.95			Units:	barrels/hr		
Is Tank Heated?:	No							
SCC Codes: List all Source	ce Classification Code(s	(SCC) that o	lescribe the	process(es	) performed	by the emission		
source (e.g., 1-02-002-0	4).							
		1-00-1	10-20					
<b>Potential Operating Sc</b>	<b>hedule:</b> Provide the	operating sc	hedule for t	his emissio	n unit.			
Hours/day:		24						
Hours/year:		8760		•				
				-				

Control Equipment: Yes								
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.								
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?								
☐ Yes ✓ No								
Pollutant:								
Proposed BACT:								
*If yes, attach BACT Analysis with this application.								
Louiset Ashievahla Emissian Data (LAED), Was a LAED Analysis annulated Coulting and 12								
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?  Yes  No								
Pollutant:								
Proposed LAER:								
*If yes, attach LAER Analysis with this application.								
if yes, attach Exerciselysis with this application.								
Federal and State Rule Applicability:								
New Source Performance Standards (NSPS): Subject, but exempt								
New Source Performance Standard are listed under 40 CFR 60-								
Standards of Performance for New Stationary Sources.								
NSPS Subpart: 0000								
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected								
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR								
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).								
Part 61 NESHAP Subpart:								
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected								
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63								
Part 63 NESHAP Subpart:								
Prevention of Significant Deterioration (PSD):  Not Affected								
These rules are found under WAQSR Chapter 6, Section 4.								
Non-Attainment New Source Review: Not Affected								
These rules are found under WAQSR Chapter 6, Section 13.								

OILTNK 1-4 2TH

**Emissions Information-** The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

**Efficiency Standards** Pre-Controlled Potential Potential Potential Potential Emissions to Emit to Emit to Emit Basis for (PTE) (lbs/hr) (tons/yr) Units (tons/yr) Determination Criteria Pollutants: 1.) Particulate emissions (PE/PM) (formerly particulate matter, PM) 2.) PM #10 microns in diameter (PE/PM10) 3.) PM #2.5 microns in diameter (PE/PM2.5) 4.) Sulfur dioxide (SO2) 5.) Nitrogen Oxides (NOx) 6.) Carbon monoxide (CO) 7.) Volatile organic 1.245 0.006 0.025 **Tanks Program** compounds (VOC) 8.) Lead (Pb) 9.) Total Hazrdous Air 0.02 0 Tanks Program Pollutants (HAPs) 10.) Fluoride (F) 11.) Hydrogen Sulfide (H2S) 12.) Mercury (Hg) 13.) Total Reduced Sulfur (TRS) 14.) Sulfuric Acid Mist (SAM)

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	Efficiency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

			Effic	ciency Standards			
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	,					***************************************	
1.)							
2.)							
3.)							
4.)							
5.)							
6.)							
7.)							
8.)							

## Storage Tank/Silo

Company Equipment ID:	WTRNK 1-2 1TH						
Company Equipment Des	cription:		2 x	400 bbl Wa	ter Storage	: Tank	
Operating Status:	Operating						
Initial Construction Comm	nencement Date:						
Initial Operation Commer	cement Date:		4/28	3/2015		<del></del>	
Most Recent Construction	n/ Modification					_	
Commencement Date:	_						
						_	
Most Recent Operation C	ommencement Date:					_	
Select reason(s) for this e	emissions unit being in	cluded in 1	this applica	tion (must l	be complete	ed regardless of date of	
installation or modification				_			
Reason:	Construction (Greent	field/New	Facility)				
If reason is <i>Reconstructio</i>	<b>n</b> or <b>Temporary Permi</b>	t or Other	, please ex	plain below	:-		
				1			
	1						
	Liquid						
Description of Material St	ored:		Prod	uced Water	(1% Oil Car	rryover)	
Canacity	400		I India.	la a marella	Т		
Capacity:	400	265	Units:	barrels		L	
Maximum Hourly Through		365		_	Units:	barrels/yr	
Is Tank Heated?:	<del></del>	1			Units:	barrels/hr	
is rank Heateur:	No						
CCC Codes, List all Course	Classification Code(s) (	CCC) +b -+ .	علف مانسم	/	· \	al less the entered and	
SCC Codes: List all Source		SCC) that i	describe the	e process(es	s) performe	a by the emission	
source (e.g., 1-02-002-04)	•						
		1-00-1	10-20				
Martin Company of the		1-00-1	.10-20				
Potential Operating Sche	edule: Provide the o	nerating so	hedule for	this emission	n unit		
Hours/day:	Trovide the of	24	incuaic ioi	CI 113 CI 113310	ii aiiic		
Hours/year:		8760		_			
Hours/ year.		0700					

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
Yes✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Laurent Achievelela Enginiera Data (LAED), Mara LAED A. L. i
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ☑ No
Pollutant:
Proposed LAER:  *If yes, attach LAER Analysis with this application.
if yes, attach EAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS):  Subject, but exempt
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD):  Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non Attainment New Course Project
Non-Attainment New Source Review: Not Affected  Those rules are found under IVAOSE Chapter 6. Section 12.
These rules are found under WAQSR Chapter 6, Section 13.

TRTNK 1-2 1TH

**Emissions Information-** The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

			Effic	ciency Standards			
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
riteria Po	llutants:						
1.)							
	Particulate emissions			# F			
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)						
5.)	Nitrogen Oxides						
	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic	0.018			0	0	Tanks Program
	compounds (VOC)						
8.)	Lead (Pb)						
9.)	Total Hazrdous Air	0			0	0	Tanks Program
	Pollutants (HAPs)						
10.)	Fluoride (F)						
11.)	Hydrogen Sulfide						
	(H2S)						
	Mercury (Hg)						
13.)	Total Reduced Sulfur						
	(TRS)						
14.)	Sulfuric Acid Mist						
	(0.4.4.)	I	1	I	1	1	1

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	Efficiency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

				_		
		Efficie	ency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:					-	
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

## Loading/Unloading/Dump

Company Equipment ID:		0	IL LOAD 1TH		
Company Equipment Des	cription:		Oil Loadout Facility		
Operating Status:	Operating				
Initial Construction Comm	nencement Date:				
Initial Operation Comme	ncement Date:	4/28	3/2015		
Most Recent Construction	n/ Modification				
Commencement Date:				_	
Most Recent Operation C					
Select reason(s) for this		luded in this applicat	ion (must be complete	ed regardless of date of	
installation or modificati			-		
Reason:	Construction (Green	field/New Facility)			
If reason is Reconstruction	on or Temporary Permit	or <i>Other</i> , please exp	lain below:		
Type of Material:	quid				
Material Description:	quiu		Crude Oil		
Material Description.	-		Crude On		
Maximum Annual Throug	 ghput:	25915	Units:	barrels/yr	
Maximum Hourly Throug		240	– Units:	barrels/hr	
Detailed Description of Lo		o Source:	Crude oil is loaded from storage tanks		
into tanker trucks for tra	nsport to market. Tank	ker truck vapors are re	eturned to storage tan	ks for	
destruction in the vapor	combustor (FLR2).				
SCC Codes: List all Source	Classification Code(s) (	SCC) that describe the	process(es) performed	d by the emission source	
(e.g., 1-02-002-04).		,	. , , ,	,	
,					
		1-00-112-01			
Potential Operating Sch	edule: Provide the or	perating schedule for t	this emission unit.		
Hours/day:		24			
Hours/year:		8760	_		
• • • • • • • • • • • • • • • • • • • •			_		

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ☑ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ☑ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS):  Not Effected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63) standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD):  Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Those fules are lound under WAGON Onapier o, Section 4.
Non-Attainment New Source Review: Not Affected
Trouble transfer of the state o

Oil Loadout 1TH

Emissions Information- The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

Efficiency Standards

			Effic	ciency Standards			
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants:						•
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)						
5.)	Nitrogen Oxides						
	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic	1.44			0.0066	0.03	AP-42
	compounds (VOC)						
	Lead (Pb)						
9.)	Total Hazrdous Air						
	Pollutants (HAPs)						
10.)	Fluoride (F)						
11.)	Hydrogen Sulfide						
	(H2S)						
	Mercury (Hg)						
13.)	Total Reduced Sulfur						
	(TRS)						
14.)	Sulfuric Acid Mist						
	(SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	Efficiency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

		Efficien	ncy Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

## Loading/Unloading/Dump

Company Equipment ID:		WTR LOAD 1TH					
Company Equipment Descrip	tion:	Prod	uced Water Loadout	Facility			
Operating Status:	Operating						
Initial Construction Commend	cement Date:	American American Society and a state of the	April 10 mars at the control of the				
Initial Operation Commencer	nent Date:	4/28/	/2015	_			
Most Recent Construction/ N	1 odification						
Commencement Date:							
Most Recent Operation Com	mencement Date:						
Select reason(s) for this emis		cluded in this application	on (must be complete	— ed regardless of date of			
installation or modification)			(	- San and Cr. Made Cr.			
	onstruction (Green	field/New Facility)					
	1	, , , , , , , , , , , , , , , , , , , ,					
Type of Material: Liquic Material Description:	I	Produced W	ater w/ 1% Crude Oil	I			
Maximum Annual Throughpu		365	. Units:	barrels/yr			
Maximum Hourly Throughpu		240	Units:	barrels/hr			
Detailed Description of Loadi	ng/Unloading/Dum	p Source:	Crude oil is loaded f	rom storage tanks			
into tanker trucks for transp	ort to market. Tan	ker truck vapors are ret	turned to storage tan	ks for			
destruction in the vapor con	nbustor (FLR2).						
<b>SCC Codes:</b> List all Source Cla (e.g., 1-02-002-04).	ssification Code(s) (	SCC) that describe the p	process(es) performed	d by the emission source			
		1-00-112-01					
Potential Operating Schedu	le: Provide the o	perating schedule for th	nis amissian unit				
Hours/day:	ie. Flovide tile 0	24	ns ennssion unit.				
Hours/year:		8760	-				
поиту/уеат:	Parameter	0/00					

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Effected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61): Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

Water Loadout 1TH

Emissions Information- The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

Efficiency Standards

			Effic	ciency Standards			
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants:						
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)						
5.)	Nitrogen Oxides						
	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic	0.02			0.0001	0	AP-42
	compounds (VOC)						
	Lead (Pb)						
9.)	Total Hazrdous Air						
	Pollutants (HAPs)						
10.)	Fluoride (F)						
11.)	Hydrogen Sulfide						
	(H2S)						
12.)	Mercury (Hg)						
13.)	Total Reduced Sulfur						
	(TRS)						
14.)	Sulfuric Acid Mist						
	(SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	ciency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

		Effici	ency Standards	7		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	I and a second					
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

## **Fugitives**

Company Equipment II	):				FUG01					
Company Equipment D	escription:				Fugitive Emissions					
			<del></del>							
Operating Status:		Operating								
Initial Construction Cor						_				
Initial Operation Comm				4/28/	2015	_				
Most Recent Construct	ion/ Modif	ication								
Commencement Date:						_				
Most Recent Operation	Commend	ement Date:								
		(V)	cluded in this	annlicatio	on (must be complete	— ed regardless of date of				
3387 53		s dille bellig lile	cidaca iii tiiis	аррпсасто	iii (iiiust be complete	tu regardless of date of				
installation or modification):  Reason: Construction (Greenfield/New Facility)										
Reason:	Consti	uction (Green	rieid/New Fac	cility)						
If reason is <i>Reconstruc</i>	tion or Ten	nporary Permi	<b>t</b> or <b>Other,</b> pl	ease expla	ain below:					
Type of Fugitive Emissi	on:	Fugitiv	ve Leaks at O&	&G						
SCC Codes: List all Sour (e.g., 1-02-002-04).	ce Classific	ation Code(s) (	SCC) that des	cribe the p	process(es) performed	d by the emission source				
			1-00-115	-00						
Potential Operating S	chodulo	Provide the ex	norating scho	dula for th	is emission unit.					
at the second control of the second control		Frovide the of	- Company	uule lõi tii	is emission unit.					
Hours/day:			24							
Hours/year	:		8760							

Control Equipment: No
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ☑ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
Yes Vo No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Effected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Foliutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Talt oo Meerin a Gasparti
Prevention of Significant Deterioration (PSD):  Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

FUG1TH

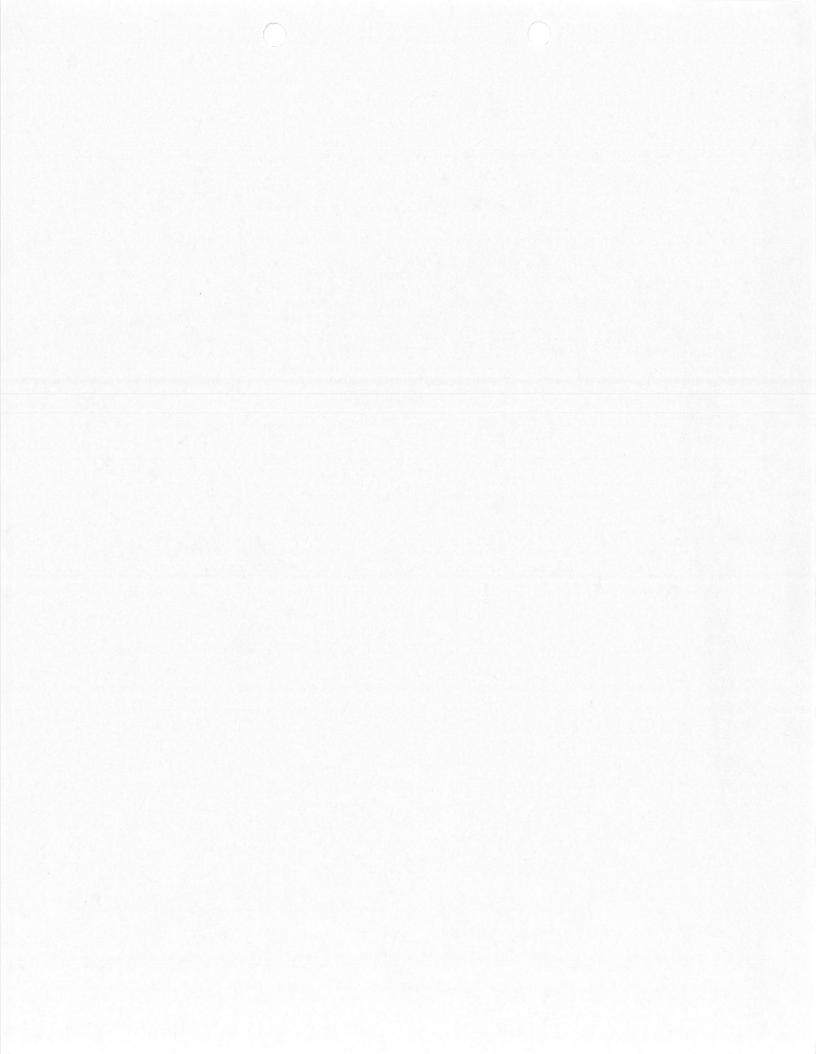
**Emissions Information-** The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

**Efficiency Standards** Potential Potential Pre-Controlled Potential to Emit to Emit to Emit Potential Emissions Basis for (PTE) (lbs/hr) (tons/yr) Determination (tons/yr) Units Criteria Pollutants: 1.) Particulate emissions (PE/PM) (formerly particulate matter, PM) 2.) PM #10 microns in diameter (PE/PM10) 3.) PM #2.5 microns in diameter (PE/PM2.5) 4.) Sulfur dioxide (SO2) 5.) Nitrogen Oxides (NOx) 6.) Carbon monoxide (CO) 7.) Volatile organic 1.302 0.297 1.302 AP-42 compounds (VOC) 8.) Lead (Pb) 9.) Total Hazrdous Air 0.002 0.0005 0.002 AP-42 Pollutants (HAPs) 10.) Fluoride (F) 11.) Hydrogen Sulfide (H2S) 12.) Mercury (Hg) 13.) Total Reduced Sulfur (TRS) 14.) Sulfuric Acid Mist (SAM)

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	iency Standards	1		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	Desire de la constante de la c					
1.)				111		
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

	9			-		
		Effic	ciency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:		A		Santa S		
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						



FORM 3	The second secon			SI	TE OF	WYOM	ING					9. AI	PI WELL NO.			
Nov. 2012		OIL A	ND GA	AS CC	NSER	VATIO	N CON	MISSION					49-	009-30	065	
				]	P. O. B	ox 2640						12.	COUNTY		13. STATE	
				Casp	er Wy	oming 82	602						CONVE	RSE	Wyon	ning
WELL	COMPLETION	OR RECON	<b>APLETI</b>	ON RE	PORT A	ND LOG	SUBMIT S	SINGLE, DUPLICA	TE ON STA	ATE LA	ND)	5. ST	ATE LEASE SE	ERIAL NO.		
1a. Type of Well	X Oil Well		Gas Well		Dry	СВМ		Other:								
b. Type of Complete	ion X	New Well	' П	Workover		Deepen		Plug Back	Γ	П	Diff. Resvr.	7. UI	NIT OR COMM	UNITIZATION	AGREEMENT	,
Initial		ı			,									17711100	14537	
Initial	Final	Ot	ther											W Y W 1800	)45X	
<ol><li>Name of Operator</li></ol>	CONVERSION   P. O. Box 24-0   P. O. Bo															
RKI EXPLO	RATION & PI	RODUCTI	ON									S	PLIT HI	LL I	UNIT 37-	68-27
3. Address							3a.	Phone No. (include	area code)			8a. V	VELL No.			
											200000000000000000000000000000000000000			1TH		
			- W WOO	<i>aa</i>	- 4	C-11-		Email: <u>hl</u>	orehm@	@rkix	A	10 1	TELD MANG			
	Report tocation clearly i	ana in accoraance	e wiin WOG	C require	ements with			12.1.150.50		1.0		10. F	IELD NAME			
At surface G	R 4553' S	WSW 35	50' FW	L 97:	5' FW	/L 83	Lat.	43.14/252	Long.	103						
Top prod. Int. TVD							Lat.	43.148637	Long,	10:	5.017226					
		VSW 85	56' FS	L 69	98' FV											68W
At total depth		W/NIW/ 11	IO' EN	II 63	11 EV		Lat.	43.160332	Long.	10:	5.016857				NO	
14. Date Spudded		***************************************		L 03	) 1 F V		npleted								GR, etc.)*	
1/3/20	015	1/	/10/201	5			D	& A 4/28/201	5 X	Rea	ady to Prod.				4553'	GR
19 Total Donth	MD	10903'	10	Dlug book	TD.	MD		10808	3'	T	20. Depth Bridge	e Plug	Set: MD			
18. Total Deptil.	TVD	6087'	15.	riug back	1.D	TVD		6089	'	$\perp$	(Requires	Prior	Approval) TVD			
21. Type Electric &	other Logs Run (Submit	1 copy and 1 LAS	S of each), C	ased and C	pen Hole, I	Btm Hole Press	Survey			22.	Was well cored?		X No	Yes	(Submit analysi	is)
	TVD 6087' TVD 6089'  Type Electric & other Logs Run (Submit 1 copy and 1 LAS of each), Cased and Open Hole, Btm Hole Press Survey  CEMENT, TVD, MD  Casing and Liner Record (Report all strings set in well)										Was DST run?		X No	Yes	(Submit report)	1
											Directional Survey	?	No	X Yes	(Submit copy, v	w/ cert.)
23. Casing a	nd Liner Record (Rep	oort all strings .	set in well)													
Hole Size	Size/ Grade	Wt. (#/f	f.)	Тор	(MD)	Bottom(	MD)	Stage Cementer	Depth	No.		Slu	rry Vol. (Bbl)	Cement To	p* Amou	ant Pulled
13.5"	10.75"J-55	40.5	#	0		175	3'				610	4	145	0		
8.75"	5.5" N-80	20#		0		1089	98'				1500	1	162	4750		
												_				
-										-		_			_	
24 Tubing	Record															
Size	Depth Set (M)	D) I				Size	De	pth Set (MD)	Packer	Depth (	MD) Siz	ze .	Depth	h Set (MD)	Packer Dep	pth (MD)
			5840	)'												
25. Produci			Т	·n	Г г	Oattom	26.				Simo		la of Holos		Dawf Status	
A)							1			$\dashv$		<u> </u>				
B)										$\neg$	3 1/8"					
В)							1	0110'- 1026	52'		3 1/8"		32			
B)									-							
В)										_	, -	<u> </u>				
B)										+		_				
Casper Wyoming 82602   WELL COMPLETION OR RECOMPLETION REPORT AND LOG (SUBMITSINGLE DUPLICATE			+		-											
			-				-			+	THE RESERVE OF THE PERSON NAMED IN COLUMN 1	-				
										+						
										$\top$						
-															ACTIVE	
В)																
B)										_		_				
									-	+		_				
			_					0030-0730		+	J 1/0	-	34		ACTIVE	
	nmary:	Total F	rac Stage	es:	17	Total Slur	ry (bbls)	:	36,63	33 T	Total Proppant (lb	os)			1,549.7	760
28. Product	ion- Interval A		25. Form	nation:	TEA	APOT			Product	tive Int	terval:	6,0				
Date First Produced	Test Date	Hour		Test	Production	Oil Bbl	20000	Gas MCF			il Gravity Corr. API		Gas Gravity	Flowbac		
							49									
				24 H	r. Rate		10							10.0000		NC
64/64	PSI 23	30	160			5	49	256	123:	5	467		2739	P	RODUCI	NG

29. Disposition of Gas (So.		ed, etc.)		Test Witness	:					
20 G CP 7	SOLD									
30. Summary of Porous Zo						31. Formation (Log) Markers:				
Show all important zones of time tool open, flowing and			rvals and all drill-stem tests,	including depth interval tested	, cushion used,	TEAPOT				
Formation	Тор	Bottom	Descr	iptions Contents, Etc.		Name		TVD		
TEAPOT	6493'	10758'	OIL-GAS-WAT	ER		FOX HILLS		4638'		
						LEWIS		4813'		
						TECKLA		5550'		
						TEAPOT		6093'		
						TEM OT		0073		
32. Additional remarks; in-	L clude plugging proced	ure (Req. prio	r approval):							
				E 37-70-3-2 SWD / 1,745 IN	TO REIHLE 37	7-70-3-3 SWD				
33. Indicate which items ha	ave been attached by p	lacing a check	in the appropriate boxe	s:						
X Electrical/ Mechanica	al Logs (1 full set) Cased &	& Open hole.		Geologic Report		DST Report	X Directional Surv	vey w/ Certification		
Sundry Notice for plu	agging and cementing			Core Analysis		Press. Survey	X Other: PLA	AT, FORM 10, CEMENT, BHL,		
				]			X	CAS		
34. I hereby certify that the	e foregoing and attach	ed information	n is complete and correc	t as determined from all a	vailable reco	ords (see attached instructions)*				
							~~			
Name (please print)	HEATHER B	REHM			Title <u>F</u>	REGULATORY ANALY	ST			
Signature					Date					
				INSTRUCT	IONS					
If not filed prior to the ti	ime this summary re	ecord is subn	nitted, copies of all cu			eologists, sample and core analys	sis, all types electr	ic, etc.), formation and		

If not filed prior to the time this summary record is submitted, copies of all currently available logs (drillers, geologists, sample and core analysis, all types electric, etc.), formation and pressure tests, and directional surveys should be attached hereto, to the extent required by applicable Federal and or State laws and regulations. All attachments should be listed on this form, see space 33.

Space 4: If there are no applicable State requirements, locations on Federal or Indian land should be described in accordance with Federal requirements. Please note all Lat./ Longs. In NAD 83. Calculate all "Top of Producing Intervals" and "BHL" first as distance from the section corner, second as the Lat. /Long. Spacing orders are based on a well location in a section. Well locations must match the surveyed footages.

Space 17: Indicate elevation used for depth measurements given in other spaces on this form and in any attachments.

Space 23: "Sacks Cement": Attached supplemental records for this well should show the details of any multiple stage cementing and the location of the cementing tool. Show how reported top(s) of cement were determined, i.e. circulated (CIR), or calculated (CAL), or cement bond log (CBL), or temperature survey (TS).

Spaces 25 and 28: If this well is completed for commingled production from more than one pool (multiple zone completion), state in space 25 and 26, and in space 25 show the producing interval, or intervals, top(s), bottom(s) and name(s) (if any) for the pools reported in space 28 through 28c. Submit a separate completion report on this form for each pool separately produced, (not commingled).

Space 27: If a well was fracture treated or stimulated, all data required in Chapter 3, Section 45 must be filed with this Completion Report.

#### Space 27: If a well was fracture treated or stimulated, provide Summary Data for # of Stages, Total Slurry, Total Proppant

- Space 28: Provide well test data for each interval tested or stimulated and flowed.
- Space 32: Provide frac flowback disposal volumes and handling and disposal site.
- Space 32: Provide final annulus casing pressure.

\* See instructions and spaces for additional data on page 2

Space 32 or Attachment: Provide all Stimulation Chemicals by Name, Type, Volumes and CAS #s.

Attach a wellbore diagram whenever possible.

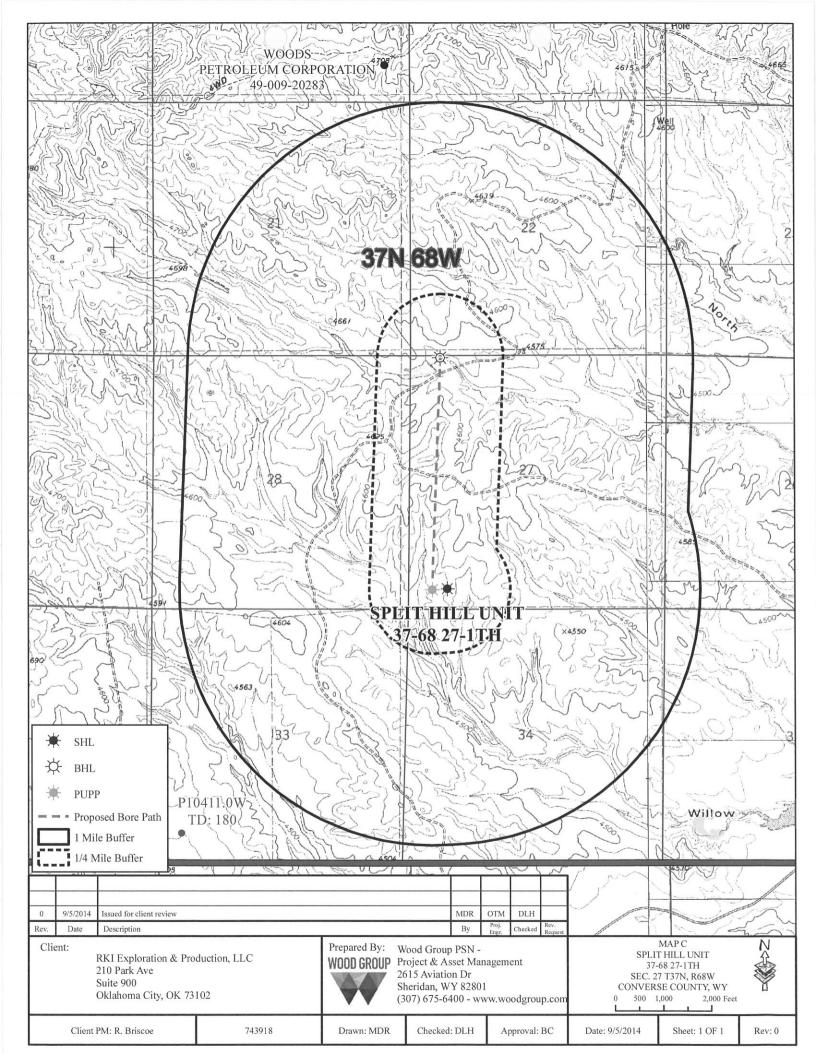
Form 10 DECEMBER, 2000 STATE OF WYOMING

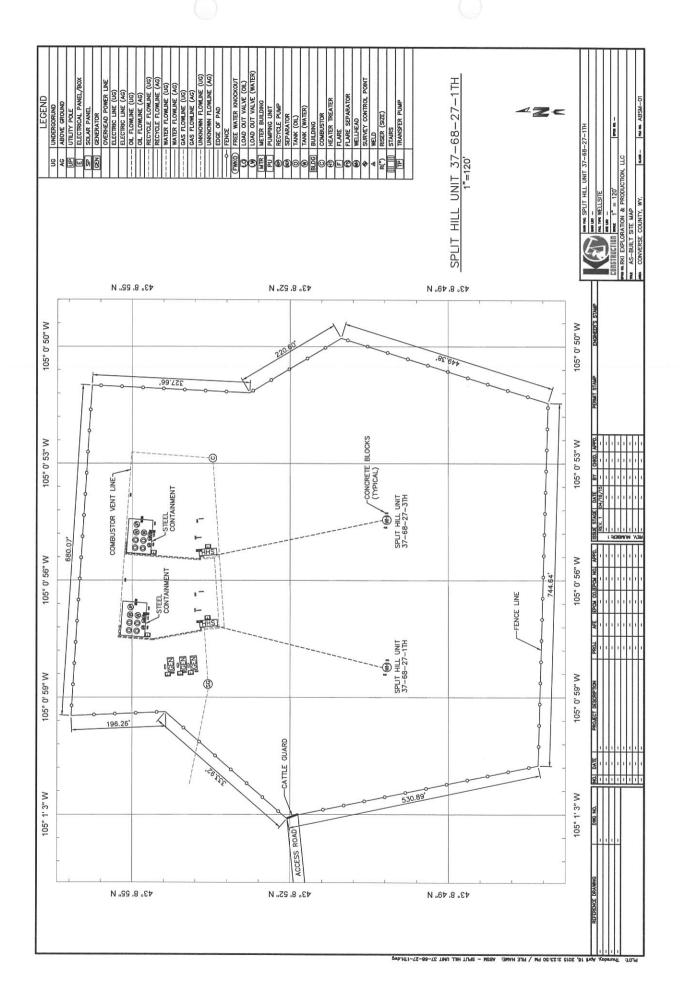
#### OIL AND GAS CONSERVATION COMMISSION

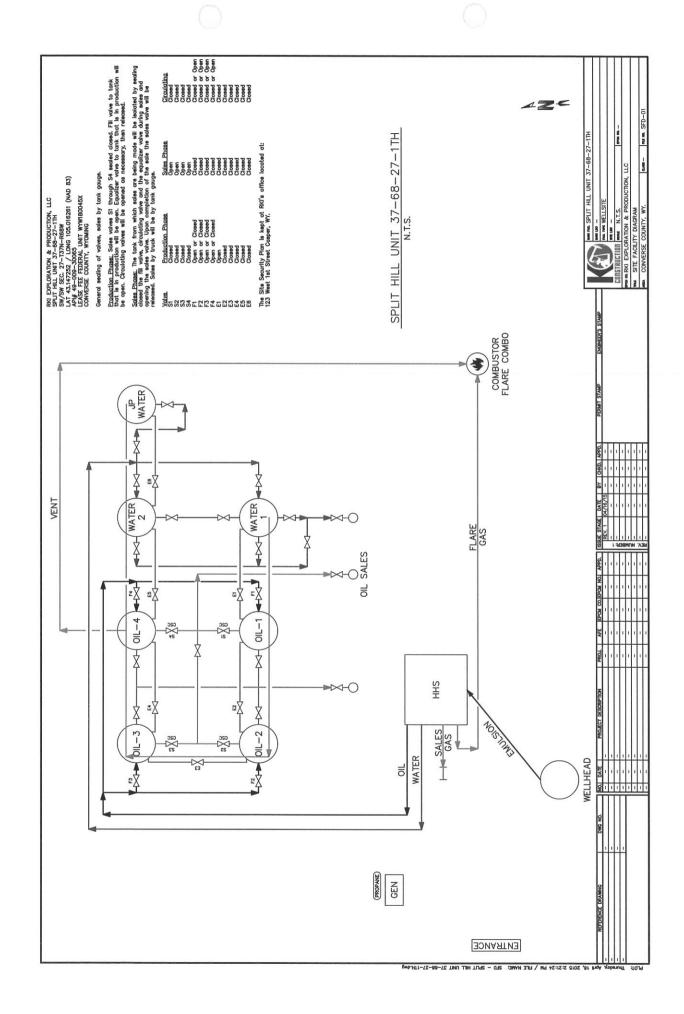
Office of State Oil and Gas Supervisor

			P.O.	Box 2640 yoming 826		V1501			
	PRODUCT					RATIO	REPORT	1	
OPERATOR							API NUMBER		
RKI EXPLORATION AND I	PRODUCTION						49-009-30065	i	
ADDRESS							WELL NAME &	NUMBER	
210 PARK AVE., SUITE 900							CDITTIIIIII	NUT 27 (0 27 17)	T
OKLAHOMA CITY, OK 73012 LEASE NAME	RI	ESERVOIR					FIELD	NIT 37-68 27-1TF	L
SPLIT HILL UNIT			TE	EAPOT				WILDCAT	
LOCATION,(quarter-quarter and foo	tages): LATITUI	DE: 43.14		LONGITUDE:	_	105.016261°	COUNTY	WILDCAT	
SW/SW 350' FSL	975' FWL	Sec. 27	, Twp.	37 N	, Rge.	. 68 W		CONVER	RSE
			TEST	Γ DATA					
START OF TEST-DATE	TIME	END OF TEST			TIME	3	DURATION OF	TEST	
5/9/2015	12:00 PM	5	/10/2015			12:00 PM		24 HRS	
TUBING PRESSURE	CASING PRESSURI	E SEPA	RATOR PR	ESSURE	S	SEPARATOR TE	MP.	CHOKE SIZE	
230	160		10	00		10:	5°F	64/6	54
OIL PRODUCTION DURING TEST		GAS PRODUC	TION DUR	ING TEST			WATER PRODU	ICTION DURING T	EST
549.28	bbls.		256.66			1CF	1 23	35.07 b	bls.
OIL GRAVITY	DOIS.	PRODUCING I					1,20	ь	DIS.
40 *API					Е	SP			
		GA	S PRO	DDUCT	OI	N			
METER MANUFACTURER							ORIFICE WELL	TESTER	X
TOTAL FLOW	Flange Tap	X PIPE TA	.P	L-10			CRITICAL FLOV	W PROVER	
ORIFICE DIAMETER		PIPE DIAMET	ER (Inside o	dia.)			ORIFICE DIAME		
1				2.067				1	
DIFFERENTIAL PRESSURE RANG	ΞE	MAX. STATIC	PRESSUR	E RANGE			PIPE DIAMETEI	R	
0-400				0-1500				2	
GAS GRAVITY (Air-1.0)		FLOWING,TE	MPERATU!	RE			GAS GRAVITY	(Air-1.0)	
0.88893 Meas.	Est X			79°F			0.88893	Meas.	Est X
DIFFERENTIAL NO FLOW READI		STATIC NO FI	OW READ	DING			24 HOUR COEF		
-0.016				12.57				N/A	
DIFFERENTIAL		STATIC					PRESSURE:	(Indicate Units	)
31				27				PSIG	
			TEST I	RESUL	TS				
DAILY OIL	DAILY WATER	?		DAILY GAS			GAS- OIL R	ATIO	
549 bbls.	1,2	35 bb	la.	2.	56.66	5 MCF	8	467.27	SCF/STB
I hereby, swear or affirm that									
rules, regulations and Instruc	tions of the Wyomi	ing Oil and Gas	Conservati	on Commiss		IGNATURE	Ada	moh	
					Т	TTLE	CD DDOD!	ICTION ENGIN	EED
					-	DATE -		ICTION ENGIN	EEK
CUDALT LOOPY COM					D			5/14/2015	
SUBMIT I COPY ONLY									

8110			70	21	22	23	4	1.9	20	21 Lette 35 for	22
		oosed Facili		28	27 <b>3N-68</b> 1	26″	25	30	29	28	ield Road
***		1,551)Ft. 94.0 Rods		33	.34	35	36	31	32	33	X 37
1111	Proposed We			4	3	2		6	5 👵	4	3
	Access Ro 12,247 ft 742.2/Ro	7.N	7	9.	10_	11-5	12	7	8	9	1(
15 14	13	18	17	16	15	14	13	18	173	16	
22 23	24-	19	20 .	<b>37N</b>		23 Well Pad		19 Walke	20 Creek I	21 Road	2
28 27 - 26.	25		AND THE RESERVE	ILL UNI	2,247 ft -	s-Road— 742.2 Ro 26	ds)	30	29	28	2
3 34 35	36	31	32	7-1 <b>-3</b> -TH-	34	35	36	31	32	33	3
3 2		6	5-5	4	3	2	1	6	5	4	3
10 11	12	7	8	9	10	. 11	12	7	8	9	1
6 15 14	13	182	17	16	15	14.*	13	_ 18	17	16	1
<b>36N</b> (21 22 23		19	20	30 N	22	23	24	1.9	36N 6	21	2
1 Laws Davides W	VV handing parts	Driving I			toly 11 7 mile			₩ Wel	l Locatio	n	2
Leave Douglas, W     Turn east onto Wa     Turn west onto pr	alker Creek road	for approximat	ely 30.9 1	miles.				=== Proj	posed Acc sting Acc		
0 9/5/2014 Issued to c Rev. Date Description	lient for review.					Dec.	DLH BC Rev. Recked Request		inty Road l Pad		
Client:  RKI Expl 210 Park Suite 900	loration & Product Ave	ion, LLC		Prepared By:	Wood Group I Project & Assa 2615 Aviation Sheridan, WY (307) 675-640	PSN - et Managemen Dr	t	SP. 3 SEC	ACCESS MAP LIT HILL UNIT 7-68 27-1,3TH 27, T37N, R68 ERSE COUNTY 6,000	W	N
Land Agent: R. Bı	riscoe	743918		Drawn: JDB	Checked: I	OLH Appr	oval: BC	9/5/2014	Sheet: 1	OF 1 F	Rev: 0





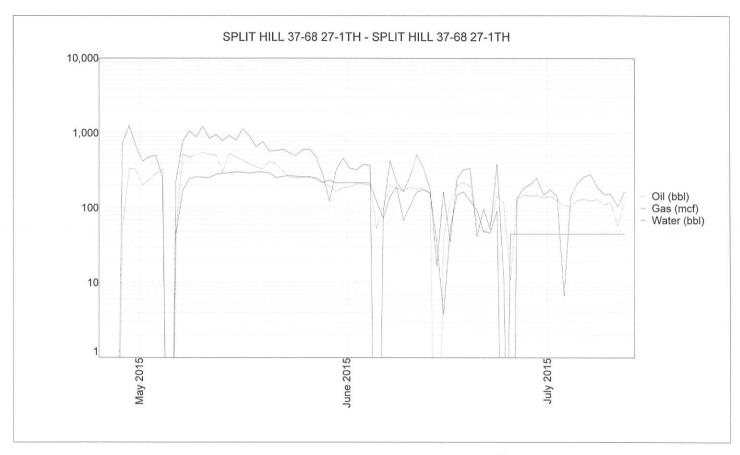




### Daily Production Report Time: SPLIT HILL 37-68 27-1TH - SPLIT HILL 37-68 27-1TH

Date: 7/13/2015 Time: 7:45 AM

Selected Time Frame: 06/25/2015 - 07/13/2015



Daily Production				Notes <dt> = Down Time</dt>
Date	Oil	Gas	Water	<gm> = Gas Meter</gm>
07/13/2015	OII	Ous	water	TOMP - Gas Meter
07/12/2015	120.86	45	165.01	
07/11/2015	57.51	45	105.00	<dt> Automation/ESD, Well shut down on</dt>
				vibration murphy fixed and back online
07/10/2015	116.69	45	151.67	
07/09/2015	111.69	45	151.66	
07/08/2015	130.03	45	188.29	
07/07/2015	124.19	45	280.06	
07/06/2015	130.86	45	260.00	
07/05/2015	126.69	45	213.33	
07/04/2015	105.02	45	141.67	
07/03/2015	107.52	45	6.67	
07/02/2015	126.69	45	141.67	
07/01/2015	143.78	45	176.65	
06/30/2015	136.69	45	148.34	
06/29/2015	149.20	45	250.00	
06/28/2015	145.03	45	206.66	
06/27/2015	149.20	45	183.37	
06/26/2015	133.36	45	135.00	<dt> Automation/ESD, Well shut down on</dt>
				vibration murphy fixed and back online
06/25/2015	10.84	45	0.00	<dt> Workover, Started well this morning</dt>



### Daily Production Report Date: 7/13/2015 Time: 7:45 AM SPLIT HILL 37-68 27-1TH

Selected Time Frame: 06/25/2015 - 07/13/2015

Daily Production Date	Oil	Gas	Water	Notes <dt> = Down Time <gm> = Gas Meter 9am on jet pump</gm></dt>
Total:	2,125.84	810	2,905.02	odin on jot pump
Average:	118.10	45	161.39	
0.6 X AUE	71	27	71	

RKI Exploration & Production, LLC Split Hill 37-68-27 PAD 1TH (Teapot Formation) sw sw 27-37N-68W Converse County, Wyoming

## Heater Treater (HTR01)

Run time (hrs): 8,760

Burner Size: 0.500 MMBtu/hr

Fuel Heat Value: 1,020 btu/scf

					Potential Em	missions (tpy)				
	NOx	CO	VOC	202	PM10	H2S	HAPs	C02	Methane	N20
HTR-1	0.21	0.18	0.01	00.00	0.02	0.00	00.00	257.65	0.00	0.00

					Potential Emissions (lb/hr)	issions (lb/hr	(			
	NOx	00	VOC	202	PM10	H2S	HAPs	C02	Methane	N20
HTR-1	0.049	0.041	0.001	00:00	0.004	0.000	0.000	58.8235294	58.8235294 0.00112745	5 0.00107843

Emission Factors (AP42 1.4 - Natural Gas Combustion)

	lb/MMscf	lb/MMscf   lb/MMBtu	
NOx	100	0.09803922	AP-42 Table 1.4-1
00	84	0.08235294	AP-42 Table 1.4-1
VOC	5.5	0.00539216	AP-42 Table 1.4-2
PM	7.6	0.00745098	AP-42 Table 1.4-2
502	09.0	0.00058824	AP-42 Table 1.4-2
C02	120000	117.647059	AP-42 Table 1.4-2
Methane	2.3	0.0022549	AP-42 Table 1.4-2
N2O	2.2	0.00215686	AP-42 Table 1.4-2

```
**************************
   Project Setup Information
*********************************
Project File : M:\Users\JIngerson\Wyoming Air Applications\Split Hill 37-68-27 PAD\Split Hill
Calculation Method : RVP Distillation
Control Efficiency : 98.0%
Known Separation
                 : Oil Tank with Separator
Known Separator Stream : Low Pressure Oil
Entering Air Composition : No
Filed Name
                 : Powder River Basin, Wyoming
Well Name
                 : Split Hill 37-68-27 1TH Oil
Well ID
                 : 49-009-30065
                 : 2015.07.13
Date
* Data Input
********************
                 : 85.00[psig]
Separator Pressure
Separator Temperature
                 : 100.00[F]
                 : 12.50[psia]
Ambient Pressure
Ambient Temperature
                : 55.00[F]
                 : 0.80927
C10+ SG
C10+ MW
                 : 227.567
No. Component
                     mol %
      H2S
  1
                      0.0000
      02
                      0.0000
  2
  3
      C02
                      0.0640
      N2
  4
                     0.0130
  5
      C1
                      0.6320
  6
      C2
                     0.1430
  7
      C3
                     0.8760
  8
      i-C4
                     0.9670
  9
      n-C4
                     2.5800
  10
      i-C5
                     1.4320
  11
      n-C5
                     1.8450
  12
      C6
                     1.6680
  13
      C7
                     6.4210
  14
      C8
                     16.5700
  15
      C9
                    11.7380
      C10+
  16
                    51.0870
  17
      Benzene
                     0.1240
  18
      Toluene
                     0.4620
  19
      E-Benzene
                     0.1390
     Xylenes
  20
                     1.6590
  21
      n-C6
                     1.2780
      224Trimethylp
                     0.3020
-- Sales Oil ------
Production Rate : 71[bbl/day]
Days of Annual Operation : 365 [days/year]
API Gravity
                 : 40.6
Reid Vapor Pressure
                 : 6.80[psia]
*******************************
   Calculation Results
-- Emission Summary ------
Item
             Uncontrolled Uncontrolled Controlled Controlled
                       [lb/hr] [ton/yr]
                                            [lb/hr]
             [ton/yr]
```

Tot	al HAPs	0.020	)	0.005	0.00	0	0.000		
	al HC	2.46		0.563	0.04		0.011		
VOC	s, C2+	1.37	7	0.314	0.02	8	0.006		
VOC	s, C3+	1.245	5	0.284	0.02	5	0.006		
Unc	ontrolled Recove								
	Vapor		2600 x1E-3						
	HC Vapor		3400 x1E-3	773					
	GOR	2.92		[SCF/bbl]					
samon d	Waississ Commoni								
No	Emission Composi Component		ntrolled	Uncontrol	lod Cont	rolled	Controlled		
NO	Component	[ton,		[lb/hr]		/yr]	[lb/hr]	1	
1	H2S	0.000		0.000	0.00	N.,	0.000		
2	02	0.000		0.000	0.00		0.000		
3	CO2	0.14		0.033	0.14		0.033		
4	N2	0.063		0.014	0.06		0.014		
5	C1	1.090		0.249	0.02		0.005		
6	C2	0.132	2	0.030	0.00	3	0.001		
7	C3	0.36	5	0.083	0.00	7	0.002		
8	i-C4	0.202	2	0.046	0.00	4	0.001		
9	n-C4	0.37		0.086	0.00	8	0.002		
10	i-C5	0.093		0.021	0.00		0.000		
11	n-C5	0.088		0.020	0.00		0.000		
12	C6	0.02		0.006	0.00		0.000		
13 14	C7	0.03		0.008	0.00		0.000		
15	C8 C9	0.03		0.007	0.00		0.000		
16	C10+	0.000		0.002	0.00		0.000		
17	Benzene	0.00		0.000	0.00		0.000		
18	Toluene	0.00		0.000	0.00		0.000		
19	E-Benzene	0.000		0.000	0.00		0.000		
20	Xylenes	0.002		0.000	0.00		0.000		
21	n-C6	0.01	5 .	0.003	0.00	0	0.000		
22	224Trimethylp	0.002	2	0.000	0.00	0	0.000		
22	224Trimethylp Total	0.002 2.67		0.000 0.611	0.00		0.000 0.012		
	Total	2.67	4						
	Total Stream Data	2.67	4	0.611	0.05	3	0.012		matal Painting
	Total	2.67	4	0.611 LP Oil	0.05	3  . Sale Oil	0.012  Flash Gas		Total Emissions
 No.	Total Stream Data Component	2.67	4  MW	0.611 LP Oil mol %	0.05 Flash Oil	Sale Oil	0.012 Flash Gas mol %	mol %	mol %
 No.	Total Stream Data Component H2S	2.67	4 MW 34.80	0.611 LP Oil mol % 0.0000	0.05 Flash Oil mol % 0.0000	Sale Oil mol % 0.0000	0.012 Flash Gas mol % 0.0000	mol % 0.0000	mol % 0.0000
 No. 1 2	Total Stream Data Component H2S O2	2.67	4 MW 34.80 32.00	0.611 LP Oil mol % 0.0000 0.0000	0.05  Flash Oil  mol % 0.0000 0.0000	Sale Oil mol % 0.0000 0.0000	0.012 Flash Gas mol % 0.0000 0.0000	mol % 0.0000 0.0000	mol % 0.0000 0.0000
 No.	Total Stream Data Component H2S	2.67	4 MW 34.80	0.611 LP Oil mol % 0.0000	0.05 Flash Oil mol % 0.0000	Sale Oil mol % 0.0000	0.012 Flash Gas mol % 0.0000	mol % 0.0000	mol % 0.0000 0.0000 3.3146
 No. 1 2 3	Total Stream Data Component H2S O2 CO2	2.67	14 MW 34.80 32.00 44.01	0.611 LP Oil mol % 0.0000 0.0000 0.0640	0.05  Flash Oil mol % 0.0000 0.0000 0.0492	Sale Oil mol % 0.0000 0.0000 0.0492	0.012 Flash Gas mol % 0.0000 0.0000 3.3146	mol % 0.0000 0.0000 0.0000	mol % 0.0000 0.0000
 No. 1 2 3	Total Stream Data Component H2S O2 CO2 N2	2.67	4  MW 34.80 32.00 44.01 28.01	0.611 LP Oil mol % 0.0000 0.0000 0.0640 0.0130	0.05 Flash Oil mol % 0.0000 0.0000 0.0492 0.0031	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031	0.012 Flash Gas mol % 0.0000 0.0000 3.3146 2.1969	mol % 0.0000 0.0000 0.0000 0.0000	mo1 % 0.0000 0.0000 3.3146 2.1969
 No. 1 2 3 4 5	Total Stream Data Component H2S O2 CO2 N2 C1	2.67	MW  34.80 32.00 44.01 28.01 16.04	0.611 LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320	0.05 Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256	0.012 Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697	mol % 0.0000 0.0000 0.0000 0.0000 0.0000	mo1 % 0.0000 0.0000 3.3146 2.1969 68.0697
No. 1 2 3 4 5 6 7 8	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12	0.611  LP Oil mol % 0.0000 0.00640 0.0130 0.6320 0.1430 0.8760 0.9670	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556	Sale Oil mol % 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556	0.012 Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mo1 % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831
 No. 1 2 3 4 5 6 7 8	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624	0.012 Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mo1 % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615
 No. 1 2 3 4 5 6 7 8 9	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15	D.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320	Flash Oil mol % 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mo1 % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957
No.  1 2 3 4 5 6 7 8 9 10 11	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15	D. 611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478	Sale Oil mol % 0.0000 0.0000 0.0492 0.031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957
No.  1 2 3 4 5 6 7 8 9 10 11 12	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16	D.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.25624 1.4326 1.8478 1.6742	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049
 No. 1 2 3 4 5 6 7 8 9 10 11 12 13	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20	D.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485	Sale Oil mol % 0.0000 0.0000 0.0492 0.031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23	D.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28	D.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380	Flash Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57	0.611  LP Oil mol % 0.0000 0.00640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870	Flash Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28	D.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380	Flash Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648
 No. 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240	Flash Oil mol % 0.0000 0.0000 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620	Flash Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 11.7380 51.0870 0.1240 0.4620 0.1390	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18	0.611  LP Oil mol % 0.0000 0.00640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Total  Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6550 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033 166.44	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp  MW Stream Mole Rat	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	0.611  LP Oil mol % 0.0000 0.00640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp  MW Stream Mole Rat Heating Value	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 106.17 86.18 114.24  [BTU/SCF]	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6550 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033 166.44	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136  26.79 0.0045 1466.18	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136  26.79 0.0045 1466.18
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Total  Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp  MW Stream Mole Rat	2.67	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	0.611  LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6550 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.00492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033 166.44	0.012  Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136

RVP @ 100F [psia] 7.63 6.24 6.24 Spec. Gravity @ 100F 0.705 0.705 0.705

```
Project Setup Information
*************************************
Colculation Method : RVP Distillation

Control Efficiency : 00 00
Project File
               : M:\Users\JIngerson\Wyoming Air Applications\Split Hill 37-68-27 PAD\Split Hill
Known Separator Stream : Low Pressure Oil
Entering Air Composition : No
Filed Name
                  : Powder River Basin, Wyoming
Well Name
                  : Split Hill 37-68-27 1TH Water @ 1% Oil
Well ID
                  : 49-009-30065
Date
                  : 2015.07.13
*****************************
* Data Input
                 : 85.00[psig]
Separator Pressure
Separator Temperature
                  : 100.00[F]
                  : 12.50[psia]
Ambient Pressure
                 : 55.00[F]
Ambient Temperature
                 : 0.80927
C10+ SG
C10+ MW
                  : 227.567
-- Low Pressure Oil ------
  No. Component
                     mol %
  1
       H2S
                      0.0000
  2
      02
                      0.0000
  3
      CO2
                      0.0640
  4
      N2
                      0.0130
  5
      C1
                      0.6320
  6
      C2
                      0.1430
  7
      C3
                      0.8760
  8
      i-C4
                      0.9670
  9
      n-C4
                      2.5800
  10
      i-C5
                      1.4320
  11
      n-C5
                      1.8450
  12
      C6
                      1.6680
  13
      C7
                      6.4210
  14
       C8
                      16.5700
  15
      C9
                      11.7380
  16
      C10+
                     51.0870
  17
      Benzene
                      0.1240
  18
       Toluene
                      0.4620
  19
       E-Benzene
                      0.1390
  20
      Xylenes
                      1.6590
  21
      n-C6
                      1.2780
  22
      224Trimethylp
                      0.3020
-- Sales Oil ------
Production Rate : 1[bbl/day]
Days of Annual Operation : 365 [days/year]
               : 40.6
API Gravity
Reid Vapor Pressure
                  : 6.80[psia]
*************************************
   Calculation Results
-- Emission Summary ------
              Uncontrolled Uncontrolled Controlled Controlled
              [ton/yr]
                        [lb/hr]
                               [ton/yr]
                                              [lb/hr]
```

				19 010		NOT COUNTY		
	al HAPs	0.000	0.000	0.00		0.000		
	al HC s, C2+	0.035 0.019	0.008	0.00		0.000		
	s, C3+	0.019	0.004	0.00		0.000		
,,,,	,	0.010	0.004	0.00		0.000		
Unc	ontrolled Recove	ry Info.						
	Vapor	2.9200 x1E-3	[MSCFD]					
	HC Vapor	2.7600 x1E-3	[MSCFD]					
	GOR	2.92	[SCF/bbl]					
	Emission Composi	1:						
No	Component	Uncontrolled	Uncontrol	led Cont	rolled	Controlle		
110	component	[ton/yr]	[lb/hr]		/yr]	[lb/hr]	:u	
1	H2S	0.000	0.000	0.00		0.000		
2	02	0.000	0.000	0.00		0.000		
3	CO2	0.002	0.000	0.00		0.000		
4	N2	0.001	0.000	0.00	1	0.000		
5	C1	0.015	0.003	0.00	0	0.000		
6	C2	0.002	0.000	0.00	0	0.000		
7	C3	0.005	0.001	0.00	0	0.000		
8	i-C4	0.003	0.001	0.00		0.000		
9	n-C4	0.005	0.001	0.00		0.000		
10 11	i-C5 n-C5	0.001	0.000	0.00		0.000		
12	C6	0.001 0.000	0.000	0.00		0.000		
13	C7	0.001	0.000	0.00		0.000		
14	C8	0.000	0.000	0.00		0.000		
15	C9	0.000	0.000	0.00		0.000		
16	C10+	0.000	0.000	0.00		0.000		
17	Benzene	0.000	0.000	0.00	0	0.000		
18	Toluene	0.000	0.000	0.00	0	0.000		
19	E-Benzene	0.000	0.000	0.00	0	0.000		
20	Xylenes	0.000	0.000	0.00		0.000		
21	n-C6	0.000	0.000	0.00		0.000		
22	224Trimethylp	0.000	0.000	0.00		0.000		
	Total	0.036	0.008	0.00	1	0.000		
No.	Stream Data							
	Stream Data Component	MW	LP Oil	Flash Oil	Sale Oil	Flash Gas	W&S Gas	Total Emissions
			LP Oil	Flash Oil	Sale Oil	Flash Gas	W&S Gas	Total Emissions
1	Component H2S	MW 34.80	mol % 0.0000	mol % 0.0000				
2	Component H2S O2	MW 34.80 32.00	mol % 0.0000 0.0000	mol % 0.0000 0.0000	mol % 0.0000 0.0000	mol % 0.0000 0.0000	mol % 0.0000 0.0000	mol %
2	Component H2S O2 CO2	MW 34.80 32.00 44.01	mol % 0.0000 0.0000 0.0640	mol % 0.0000 0.0000 0.0492	mol % 0.0000 0.0000 0.0492	mol % 0.0000 0.0000 3.3146	mol % 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146
2 3 4	Component H2S O2 CO2 N2	MW 34.80 32.00 44.01 28.01	mol % 0.0000 0.0000 0.0640 0.0130	mol % 0.0000 0.0000 0.0492 0.0031	mol % 0.0000 0.0000 0.0492 0.0031	mol % 0.0000 0.0000 3.3146 2.1969	mol % 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969
2 3 4 5	Component H2S O2 CO2 N2 C1	MW 34.80 32.00 44.01 28.01 16.04	mol % 0.0000 0.0000 0.0640 0.0130 0.6320	mol % 0.0000 0.0000 0.0492 0.0031 0.3256	mol % 0.0000 0.0000 0.0492 0.0031 0.3256	mol % 0.0000 0.0000 3.3146 2.1969 68.0697	mol % 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697
2 3 4 5 6	Component H2S O2 CO2 N2 C1 C2	MW  34.80 32.00 44.01 28.01 16.04 30.07	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100
2 3 4 5 6 7	Component H2S O2 CO2 N2 C1 C2 C3	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887
2 3 4 5 6	Component H2S O2 CO2 N2 C1 C2 C3 i-C4	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831
2 3 4 5 6 7 8	Component H2S O2 CO2 N2 C1 C2 C3	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.9556 2.5624	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615
2 3 4 5 6 7 8 9	Component H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831
2 3 4 5 6 7 8 9	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957
2 3 4 5 6 7 8 9 10 11 12 13	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957
2 3 4 5 6 7 8 9 10 11 12 13 14	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049
2 3 4 5 6 7 8 9 10 11 12 13 14 15	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene E-Benzene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene  E-Benzene  Xylenes	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17	mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene  E-Benzene  Xylenes  n-C6  224Trimethylp	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 0.1396 1.6665 1.2830	mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene  E-Benzene  Xylenes  n-C6  224Trimethylp	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020 165.80	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene  E-Benzene  Xylenes  n-C6  224Trimethylp  MW  Stream Mole Rat	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene  E-Benzene  Xylenes  n-C6  224Trimethylp  MW  Stream Mole Rat Heating Value	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 186.18 114.24	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020 165.80	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136 26.79 0.0045 1466.18	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136  26.79 0.0045 1466.18
2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Component  H2S  O2  CO2  N2  C1  C2  C3  i-C4  n-C4  i-C5  n-C5  C6  C7  C8  C9  C10+  Benzene  Toluene  E-Benzene  Xylenes  n-C6  224Trimethylp  MW  Stream Mole Rat	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	mol % 0.0000 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020 165.80	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136

RVP @ 100F [psia] 7.63 6.24 6.24 Spec. Gravity @ 100F 0.705 0.705

Split Hill 37-68-27 PAD 1TH (Teapot Formation) RKI Exploration & Production, LLC Converse County, Wyoming sw sw 27-37N-68W

Oil Loadout

Model: OIL LOAD-1 Oil Truck Loadout Source ID Number: Name

Liquid Loading

1088430 0.6 365 60.00 26.82 Molecular Weight (lb/lb-mole): Saturation Factor: Throughput Value (gal/yr): 55 6.80 24 109 Liquid Temperature (°F): Vapor Pressure (psia)

Load Duration (min/truck): Days Per Year: Load Frequency (trucks/yr): Hours Per Day:

Loading Loss (lb/1000 gal) = (12.46\*S\*P\*M)/T (AP-42 Section 5.2 (1/95)) where:

S = Saturation Factor = dedicated normal service

P = True Vapor Pressure of liquid loaded\*, psia

 $M = Molecular Weight of Vapors, \ lb/lb-mole$ T = Temp. of bulk liquid loaded, deg. R = (deg. F + 460)

2.65 lb/1000 gal Loading Loss (Ib VOC/1000 gal) =

### **Uncontrolled Emissions**

Pollutant	Loading Loss	Throughput		Estimated Emissions	Source of
					<b>Emission Factor</b>
	(lb/1000 gal)	(gal/yr)	(lb/yr)	(tpy)	
VOC (includes HAPs)	2.65	1088430	2881.58	1.44	AP42
			lb/hr: 0.3289		

Source of Emission Factor Combustor Specs **Estimated Emissions** (tpy) 0.03 (lb/yr) 57.63 Loading Loss Throughput (gal/yr) 1088430 (lb/1000 gal) 0.05 Controlled Emissions Pollutant VOC (includes HAPs)

lb/hr:

# RKI Exploration & Production, LLC Split Hill 37-68-27 PAD 1TH (Teapot Formation) sw sw 27-37N-68W Converse County, Wyoming

### Water Loadout

NOTE: Throughput Value assumes 1% oil in water volume.

Liquid Loading		
Model:		; ;
WATER LOAD-1	Water Truck Loadout	
Source ID Number:	Name	

0.6 365 60.00 26.82 Molecular Weight (lb/lb-mole): Throughput Value (gal/yr): Days Per Year: Load Duration (min/truck): Saturation Factor: 55 6.80 24 2 Hours Per Day: Load Frequency (trucks/yr): Liquid Temperature (°F): Vapor Pressure (psia)

Loading Loss (lb/1000 gal) = (12.46\*5\*P\*M)/T (AP-42 Section 5.2 (1/95)) where:

S = Saturation Factor = dedicated normal service P = True Vapor Pressure of liquid loaded\*, psia

r = True Vapor Pressure of Induiu Toduceur, psia M = Molecular Weight of Vapors, Ib/Ib-mole

T = Temp. of bulk liquid loaded, deg. R = (deg. F + 460)

Loading Loss (lb VOC/1000 gal) = 2.65 lb/1000 gal

### **Uncontrolled Emissions**

Pollutant	Loading Loss	Throughput	ESI	Estimated Emissions	Source of Emission Factor
	(lb/1000 gal)	(gal/yr)	(Ib/yr)	(tpy)	
VOC (includes HAPs)	2.65	15330	40.59	0.02	AP42
			lb/hr: 0.0046		

Pollutant	Loading Loss	Throughput	Estir	stimated Emissions	Source of
	(lb/1000 gal)	(gal/yr)	(Ib/yr)	(tpy)	EIIIISSIOII FACIOI
VOC (includes HAPs)	0.05	15330	0.81	0.00	Combustor Specs

0.0001

lb/hr:

Split Hill 37-68-27 PAD 1TH (Teapot Formation) RKI Exploration & Production, LLC Converse County, Wyoming sw sw 27-37N-68W

# Fugitive Emissions (1TH FUG-1)

**Uncontrolled Emissions** 

Wt Perecent Gas:

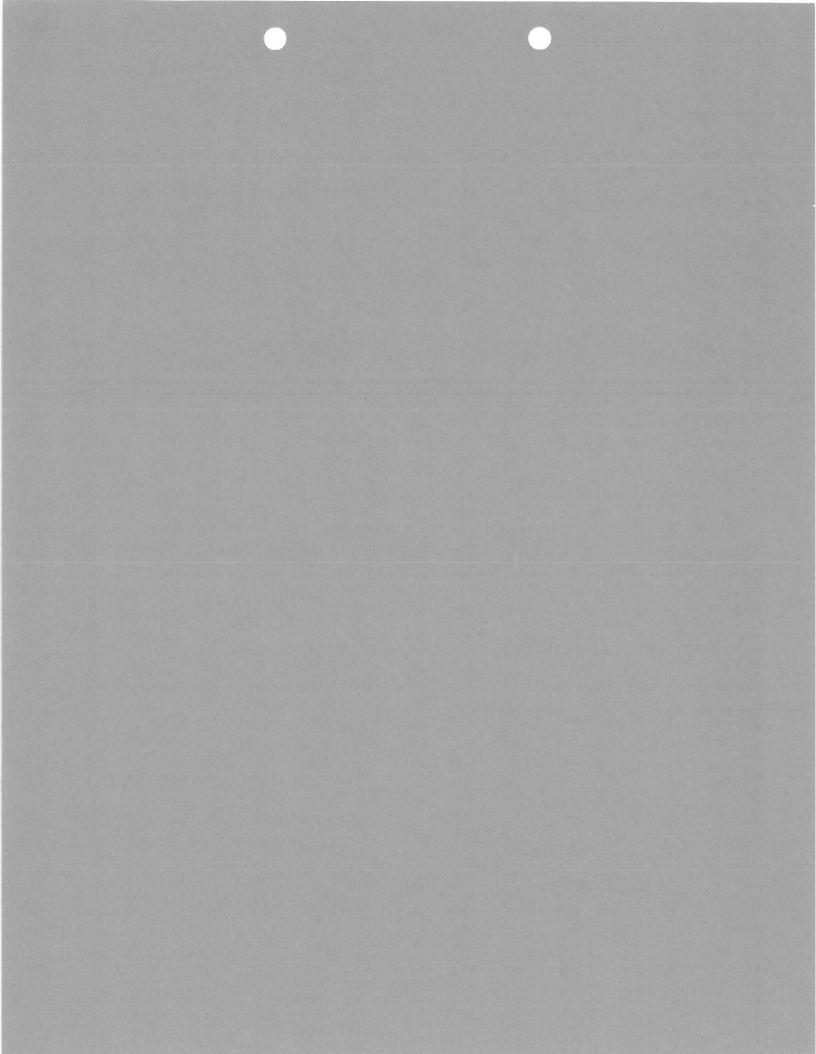
100.00 Per AMR Gas Analysis of 6/9/2014 94.79 Per AMR Gas Analysis of 6/9/2014 40.45 Per AMR Gas Analysis of 6/9/2014 1.29 Per AMR Gas Analysis of 6/9/2014

Wt Percent HC: Wt Percent VOC: Wt Percent HAPs:

									Leak Kate In I	Leak Kate in Ions Per Year	
Equipment Type	Gas Leak EF	Source	Percent	Percent	Percent	Operated	Gas Rate	Gas Rate	HC Rate	VOC Rate	HAPs Rate
	lb/hr/source	Count	HC	VOC	HAPs	Hours	lb/hr	tpy	tpy	tpy	tpy
Valves	0.005420	75	94.79	40.45	1.29	8,760	0.3853	1.688	1.600	0.683	0.001
Flanges	0.000241	118	94.79	40.45	1.29	8,760	0.0270	0.118	0.112	0.048	0.000
Connectors	0.000458	124	94.79	40.45	1.29	8,760	0.0538	0.236	0.224	0.095	0.000
Other	0.016666	17	94.79	40.45	1.29	8,760	0.2686	1.176	1.115	0.476	0.001
Open Ended Lines	0.003080	-	94.79	40.45	1.29	8,760	_	-	ı	1	1
Pumps	0.028750	-	94.79	40.45	1.29	8,760	7	1	-	1	1
Totals							0.735	3.218	3.050	1.302	0.002

Notes: See attached Gas Analysis for VOC and HAPs weight percent calculations.

Oil and Gas Production Operations leak emissions factors from EPA 453/R-95-017.



### Separator/Treater

Company Equipment ID:		HTR01 3TH				
Company Equipment Des	scription:	Horizontal Heater Treater w/ 0.500 mmbtu burner				
Operating Status:	Operating					
Initial Construction Comp	mencement Date:					
Initial Operation Commer	ncement Date:	4/28/2015				
Most Recent Construction	n/ Modification					
Commencement Date:						
Most Recent Operation C	-					
Select reason(s) for this	emissions unit being in	ncluded in this application (must be completed regardless of date				
of installation or modific	cation):					
Reason:	Construction (Green	field/New Facility)				
If reason is <i>Reconstruction</i>	on or <b>Temporary Perm</b> i	it or Other, please explain below:				
Type of Vessel:	Heater-Treater	Is Vessel Heated? Yes				
Operating Temperature (	(F):	100				
Operating Pressure (psig)	):	85				
SCC Codes: List all Source	e Classification Code(s)	(SCC) that describe the process(es) performed by the emission				
source (e.g., 1-02-002-04	.).					
		1-00-111-00				
Determine Output in a C. I	adula. Describe al	annetic a calculation this engine or with				
Potential Operating Sch	eaule: Provide the o	operating schedule for this emission unit.				
Hours/day:	***************************************	24				
Hours/year:		8760				

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Effected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD):  Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

HTR01 3TH

			Effic	iency Standards			
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants:						
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)		0.011			0.0026	0.011	AP-42
	PM #10 microns in						
	diameter (PE/PM10)						
3.)					-		
	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)	0.001			0.0002	0.001	AP-42
	Nitrogen Oxides	0.147			0.0336	0.147	AP-42
	(NOx)						
6.)	Carbon monoxide	0.123			0.0282	0.123	AP-42
	(co)					700mm 20000m 1000 100000	
7.)	Volatile organic	0.008			0.0018	0.008	AP-42
	compounds (VOC)						
8.)	Lead (Pb)						
	Total Hazrdous Air	0.003			0.0006	0.003	AP-42
33430-4	Pollutants (HAPs)	(3.20.00.000.0000)					
10.)	Fluoride (F)						
	Hydrogen Sulfide	0	1		0	0	AP-42
	(H2S)						
12.)	Mercury (Hg)						
	Total Reduced Sulfur						
,	(TRS)						
14.)	Sulfuric Acid Mist						
31117	(SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	iency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)				- 1.22		
6.)						
7.)						
8.)						

		Carried State of the Control of the				
		Effic	iency Standards	7		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

### Storage Tank/Silo

Company Equipment ID:	OILTNK 1-4 3TH					
Company Equipment Description		4 x	400 bbl Oil	Storage Ta	nks	
Operating Status:	Operating					
Initial Construction Commence						ũ
Initial Operation Commenceme			4/28/	2015		•
Most Recent Construction/ Mo	dification					
Commencement Date:						
Most Recent Operation Comme	encement Date:					
Select reason(s) for this emissi	ons unit being ir	cluded in this	application	on (must b	e complete	d regardless of date of
installation or modification):						
Reason: Con	struction (Green	field/New Faci	ility)			
If reason is <i>Reconstruction</i> or 7	Temporary Perm	it or Other, pl	ease expl	ain below:		
	, , , , , , , , , , , , , , , , , , , ,	, , , , , , , , , , , , , , , , , , , ,				
Material Type: Liquid						
Description of Material Stored:				Crud	de Oil	
Capacity: 400	)	Ur	nits:	barrels	T	
Maximum Throughput:		18615	_		Units:	barrels/yr
Maximum Hourly Throughput:		2.125	-		Units:	barrels/hr
Is Tank Heated?: No						
SCC Codes: List all Source Class	ification Code(s)	(SCC) that desc	ribe the i	orocess(es	) performed	by the emission
source (e.g., 1-02-002-04).	, ,	,		,	, ,	.,
(						
		1-00-110-	20			
		1 00 110				
Potential Operating Schedule:	Provide the c	perating sched	lule for th	nis emissio	n unit	
Hours/day:		24	ane for th	115 CITII5510	i ullici	
Hours/year:		8760				
Hours, year.		3700				

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lourset Askievable Emission Date (LAED), Was a LAED Analysis completed for this emission unit?
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?  Yes  No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
if yes, attach Each Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS):  Subject, but exempt
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart: 0000
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Environment Complete Conference Air Bulleton to (NECHAR Book CO)
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD):  Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
These false are really and the fire of the
Non-Attainment New Source Review: Not Affected

OILTNK 1-4 3TH

**Emissions Information-** The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

**Efficiency Standards** Pre-Controlled Potential Potential Potential to Emit Potential Emissions to Emit to Emit Basis for (PTE) (tons/yr) (lbs/hr) (tons/yr) Units Determination **Criteria Pollutants:** 1.) Particulate emissions (PE/PM) (formerly particulate matter, PM) 2.) PM #10 microns in diameter (PE/PM10) 3.) PM #2.5 microns in diameter (PE/PM2.5) 4.) Sulfur dioxide (SO2) 5.) Nitrogen Oxides (NOx) 6.) Carbon monoxide (CO) 7.) Volatile organic 0.543 0.002 0.011 **Tanks Program** compounds (VOC) 8.) Lead (Pb) 9.) Total Hazrdous Air 0.01 0 0 **Tanks Program** Pollutants (HAPs) 10.) Fluoride (F) 11.) Hydrogen Sulfide (H2S) 12.) Mercury (Hg) 13.) Total Reduced Sulfur (TRS) 14.) Sulfuric Acid Mist

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	iency Standards	1		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

		Efficien	ncy Standards			
	Pre-Controlled	Potential		Potential	Potential	T
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

### Storage Tank/Silo

Company Equipment ID:	WTRNK 1-2 3TH					
Company Equipment Descript	tion:		2 x	400 bbl Wa	ter Storage	Tank
Operating Status:	Operating					
Initial Construction Commend	ement Date:					
Initial Operation Commencen	nent Date:		4/28	3/2015		-
Most Recent Construction/ M	lodification					-
Commencement Date:						
	,					-
Most Recent Operation Comr	nencement Date:					
Select reason(s) for this emis	sions unit being in	cluded in	this applica	tion (must	be complete	d regardless of date of
installation or modification):						U → U Succession States Sections and Assessed
Reason: Co	nstruction (Green	field/New	Facility)			
If reason is <i>Reconstruction</i> or	Temporary Permi	it or Othe	r, please exp	plain below	:	
Material Type: Liqu	id					
Description of Material Store	d: .		Produ	uced Water	(1% Oil Car	ryover)
				,		
The state of the s	00		Units:	barrels		
Maximum Throughput:		365		_	Units:	barrels/yr
Maximum Hourly Throughput	:	1			Units:	barrels/hr
Is Tank Heated?: No	)					
SCC Codes: List all Source Class	ssification Code(s) (	(SCC) that	describe the	e process(es	s) performed	l by the emission
source (e.g., 1-02-002-04).						
		1-00-3	110-20			
Potential Operating Schedul	e: Provide the o	perating s	chedule for	this emissic	n unit.	
Hours/day:		24				
Hours/year:		8760	THE REPORT OF THE PERSON NAMED IN	<del></del>		
				-		

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Subject, but exempt
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart: 0000
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR
61. (These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD):  Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

TRTNK 1-2 3TH

*	· ·		Effic	iency Standards	7		
		Pre-Controlled	Potential	•	Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
riteria Po	llutants:						
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
,	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)						
	Nitrogen Oxides						
	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic	0.018			0	0	Tanks Program
	compounds (VOC)						3
8.)	Lead (Pb)						
	Total Hazrdous Air	0			0	0	Tanks Program
	Pollutants (HAPs)						
10.)	Fluoride (F)						
	Hydrogen Sulfide						
	(H2S)						
12.)	Mercury (Hg)						
	Total Reduced Sulfur						
	(TRS)			5.			
14.)	Sulfuric Acid Mist						
,	(SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	ciency Standards	7		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit	_	to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	-					
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

				_		
		Effic	iency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

### Loading/Unloading/Dump

Company Equipment ID	:	OIL LOAD 3TH				
Company Equipment De	escription:		Oil Loadout Facility	1		
VA 95 40 100c						
Operating Status:	Operating					
Initial Construction Com	nmencement Date:					
<b>Initial Operation Comm</b>	encement Date:		4/28/2015			
Most Recent Constructi	on/ Modification			<del></del>		
Commencement Date:				_		
Most Recent Operation	Commencement Date:					
Andrew Commence Comme		luded in this anni	ication (must be complete	— ed regardless of date of		
installation or modifica		naaca iii tiiis appi	reation (mast be complete	ea regardiess of date of		
Reason:	Construction (Green	field/New Facility				
incason.	Construction (Green	icia/ivevv racinty				
If reason is Pasanstruct	ion or Temporary Permit	or Other place	ovalaja bolovu			
ii reason is <b>Reconstruct</b>	ion of remporary Permit	of Other, please	explain below.			
	Liquid					
Material Description:			Crude Oil			
NA A I.Th		11160	11.5.	[L		
Maximum Annual Thro	-	11169	Units:	barrels/yr		
Maximum Hourly Throu	· · · · · · · · · · · · · · · · · · ·	240	Units:	barrels/hr		
man European	Loading/Unloading/Dum		Crude oil is loaded f			
		er truck vapors a	re returned to storage tan	iks for		
destruction in the vapo	or combustor (FLR2).					
SCC Codes: List all Sour	ce Classification Code(s) (	SCC) that describe	the process(es) performe	d by the emission source		
(e.g., 1-02-002-04).						
		1-00-112-01				
Potential Operating Sc	hedule: Provide the o	perating schedule	for this emission unit.			
Hours/day:		24				
Hours/year:		8760				
0000 00000 <b>. 1</b> 200000	***************************************					

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Effected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

Oil Loadout 3TH

			Efficiency Standards				
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants:						
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
	PM #2.5 microns in						
	diameter (PE/PM2.5)						
	Sulfur dioxide (SO2)						
5.)	Nitrogen Oxides						
	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic	0.62			0.0028	0.01	AP-42
	compounds (VOC)						
	Lead (Pb)						
9.)	Total Hazrdous Air						
	Pollutants (HAPs)						
	Fluoride (F)						
11.)	Hydrogen Sulfide						
	(H2S)						
	Mercury (Hg)						
13.)	Total Reduced Sulfur						
	(TRS)					-	
14.)	Sulfuric Acid Mist						
	(SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	ciency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)			18			
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

		Effic	ciency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:	-					
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)				1		

### Loading/Unloading/Dump

Company Equipment ID:		WTR LOAD 3TH				
Company Equipment Descr	iption:	Prod	uced Water Loadout F	acility		
		P0000000000000000000000000000000000000				
Operating Status:	Operating					
Initial Construction Comme				_		
Initial Operation Commence		9/7/	2014			
Most Recent Construction/	Modification					
Commencement Date:				_		
Most Recent Operation Cor	nmencement Date:					
Select reason(s) for this em		luded in this application	on (must be complete	— d regardless of date of		
installation or modification		a a b a a b a a b a a b a a b a a b a a b a a b a	m (mast ac complete	a regardiess of date of		
	Construction (Greenf	ield/New Facility)				
il do	CONSTRUCTION (OF CCIN	icia/iiciv racinty/				
If reason is <i>Reconstruction</i>	or <b>Temporary Permit</b>	or <i>Other,</i> please expla	ain below:			
Type of Material: Liqu Material Description:	id	Produced W	ater w/ 1% Crude Oil			
Maximum Annual Through	out:	365	Units:	barrels/yr		
Maximum Hourly Throughp		240	Units:	barrels/hr		
Detailed Description of Load	Went was a second and a second	Source:	Crude oil is loaded fr			
into tanker trucks for trans	port to market. Tank	er truck vapors are ret				
destruction in the vapor co						
<b>SCC Codes:</b> List all Source C (e.g., 1-02-002-04).	lassification Code(s) (S	SCC) that describe the p	process(es) performed	by the emission source		
		1 00 112-01				
Potential Operating Sched	ule: Provide the or	perating schedule for th	is emission unit			
Hours/day:	a.c. Horiac inc op	24	is chilosion and			
Hours/year:		8760	•			
			•			

Control Equipment: Yes
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
☐ Yes ✓ No
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS):  Not Effected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
Matical Engineers Chandrale for Handrale Air Ballists at (NECHAR B. 1997)
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride).
Part 61 NESHAP Subpart:
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
,
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

Water Loadout 3TH

57			Effic	iency Standards	1		
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants:						
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)						
5.)	Nitrogen Oxides						
	(NOx)						
6.)	Carbon monoxide						
	(CO)						
7.)	Volatile organic	0.02			0.0001	0	AP-42
	compounds (VOC)						
8.)	Lead (Pb)						
	Total Hazrdous Air						
	Pollutants (HAPs)						
10.)	Fluoride (F)						
	Hydrogen Sulfide				1		
1	(H2S)						
12.)	Mercury (Hg)						
	Total Reduced Sulfur						
	(TRS)						
14.)	Sulfuric Acid Mist						
	(SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

		Effic	ciency Standards	1		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

				_		
		Effic	ciency Standards	1		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

### **Fugitives**

Company Equipment ID:		FUG01				
Company Equipment Description:		Fugitive Emissions				
Operating Status:	Oper					
Initial Construction Cor						
Initial Operation Comm	nencement Date:	4/28/2015				
Most Recent Construct	ion/ Modification					
Commencement Date:		·				
Most Recent Operation	n Commencement I	Date:				
		eing included in this application (must be completed regardless of date of				
installation or modific						
Reason:		Greenfield/New Facility)				
		,,				
If reason is <i>Reconstruc</i>	<b>tion</b> or <b>Temporary</b>	Permit or Other, please explain below:				
Type of Fugitive Emissi	on:	Fugitive Leaks at O&G				
SCC Codes: List all Sour (e.g., 1-02-002-04).	rce Classification Co	de(s) (SCC) that describe the process(es) performed by the emission source				
·		1-00-115-00				
Potential Operating S	<b>chedule:</b> Provide	the operating schedule for this emission unit.				
	Hours/day: 24					
Hours/year: 8760						
nours/year						

Control Equipment: No
If yes, please fill out and attach the appropriate Control Device and Release Point Information worksheets.
Best Available Control Technology (BACT): Was a BACT Analysis completed for this emission unit?
└ Yes
Pollutant:
Proposed BACT:
*If yes, attach BACT Analysis with this application.
Lowest Achievable Emission Rate (LAER): Was a LAER Analysis completed for this emission unit?
Yes Vo
Pollutant:
Proposed LAER:
*If yes, attach LAER Analysis with this application.
Federal and State Rule Applicability:
New Source Performance Standards (NSPS): Not Effected
New Source Performance Standard are listed under 40 CFR 60-
Standards of Performance for New Stationary Sources.
NSPS Subpart:
Notice to the control of the control
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 61):  Not Effected
National Emissions Standards for Hazardous Air Pollutants (NESHAP Part 61) are listed under 40 CFR 61.
(These include asbestos, benzene, beryllium, mercury, and vinyl chloride). Part 61 NESHAP Subpart:
Part of Neshar Subpart.
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63):  Not Effected
National Emission Standards for Hazardous Air Pollutants (NESHAP Part 63)
standards are listed under 40 CFR 63
Part 63 NESHAP Subpart:
Prevention of Significant Deterioration (PSD): Not Affected
These rules are found under WAQSR Chapter 6, Section 4.
Non-Attainment New Source Review: Not Affected
These rules are found under WAQSR Chapter 6, Section 13.

FUG3TH

			Efficiency Standards				
		Pre-Controlled	Potential		Potential	Potential	
		Potential Emissions	to Emit		to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Criteria Po	llutants:	Management of the second					
1.)							
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)							
	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4.)	Sulfur dioxide (SO2)				1		
	Nitrogen Oxides						
,	(NOx)						
6.)	Carbon monoxide						
,	(co)						
7.)	Volatile organic	1.302			0.297	1.302	AP-42
	compounds (VOC)				35,077,733	877.833.833	
8.)	Lead (Pb)						
	Total Hazrdous Air	0.002			0.0005	0.002	AP-42
	Pollutants (HAPs)						
10.)	Fluoride (F)						
	Hydrogen Sulfide						
,	(H2S)						
12.1	Mercury (Hg)		1		+	1	
	Total Reduced Sulfur		1		+	1	
	(TRS)						
14 \	Sulfuric Acid Mist		<del>                                     </del>				
<u></u>	(SAM)						

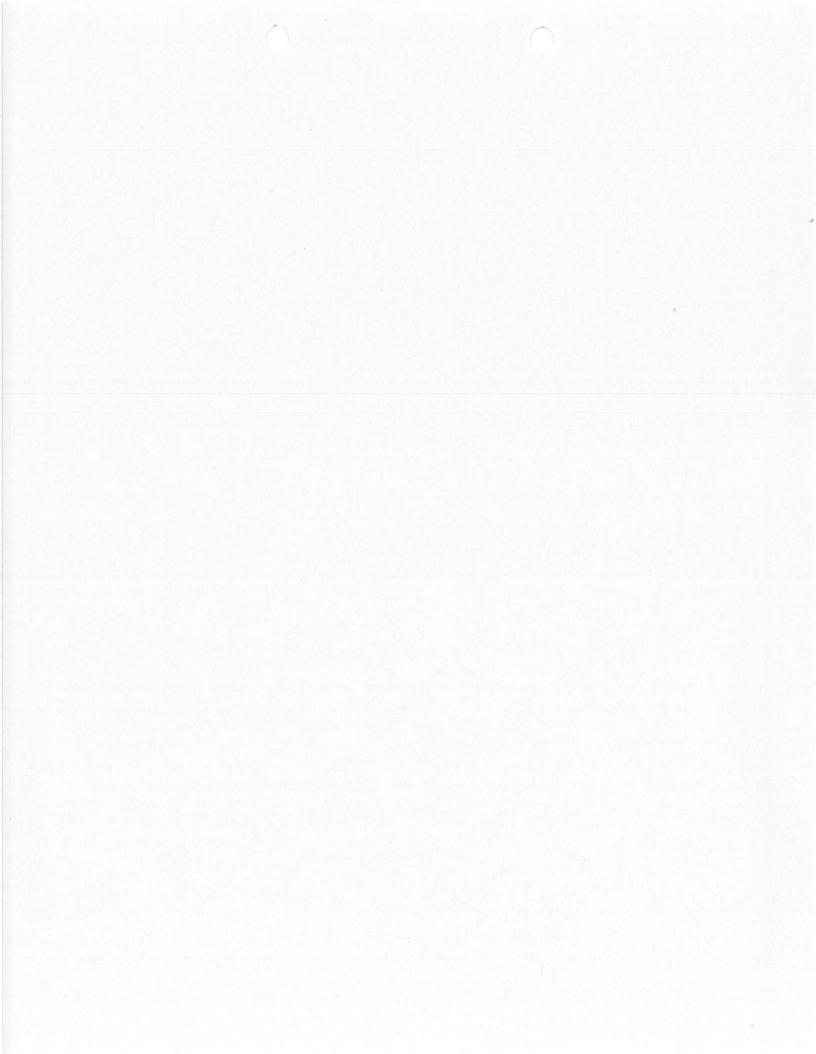
<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

### Hazardous Air Pollutants (HAPs) and Toxic Air Contaminents

		Effic	ciency Standards	7		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)			Accessed to the second			

### Greenhouse Gases (GHGs)

		Efficie	anay Ctandards	$\neg$		
			ency Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						



FORM 3				S	re of	WYOM	ING					9. API WELL	NO.		
Nov. 2012		OII	L AND G	AS C	ONSEF	RVATIO	N COI	MMISSION			7		49-00	9-30064	
				]	P. O. E	Box 2640						12. COUNT	Υ	13.	STATE
						oming 82							NVERS		Wyoming
WELL			COMPLETI	ON RE	PORT A	AND LOG (	SUBMIT S	SINGLE, DUPLICA	TE ON STA	TE LAND)		5. STATE LE	EASE SERIA	L NO.	
1a. Type of Well	X Oil Well		Gas Well		Dry	СВМ		Other:			- L				
b. Type of Complete		X New Well		Workover		Deepen		Plug Back		Diff.	Resvr.	7. UNIT OR	COMMUNIT	TIZATION AGR	REEMENT
Initial	X		Other										WY	W180045X	ζ
Name of Operator			Other									8. FARM OR	LEASE NA	ME	
RKI EXPLO	DATION &	DRODUC	TION										r HILL		T 27 60 27
	KATION &	PRODUC	TION				- 1-							UNI	T 37-68-27
<ol> <li>Address</li> <li>PARK A</li> </ol>	VE. STE. 7	00					3a.	Phone No. (include a 405.996.5769	irea code)	405.949.22		8a. WELL N	o.		
OKLAHOMA								Email: hb	rehm@	rkixp.cc	m			3TH	
Location of Well	Report location cle	early and in accor	dance with WO	GCC requir	rements wit		gtr qtrs.)					10. FIELD N	AME		
At surface G	R 4552'	SWSW	350' FW	/L 127	75' FW	/L 83	Lat,	43.147255	Long.	105.01:	137			WC	
Top prod. Int. TVD	6098'					NAD		42.140507	·	105.01		11. SEC. T, F		OCK AND SU	RVEY
М	D 6675'	SESW	833' FS	SL 20	15' FV	VL 83	Lat.	43.148587	Long.	105.012	.293	OR AREA	27	T 37N	r 68W
TV At total depth	3079(5)(5)(5)(6)					NAD	Lat.	43.160293	Long.	105.01	799	36. MULTIP	LE COMPL.	? NO	
M 14. Date Spudded		NENW 15. Date T.D. Re		VL 19	80' FV	VL 83 16. Date Con	npleted						OR AA. DA	ATE: RKB, RT, GR, et	tc.)*
12/18/2	- 1		12/27/20	14		ro. Date con		& A 4/28/201:	5 X	Ready to			10110 (01,1		52' GR
	MD	10945	5' ],,	DI 1 1		MD		10843	' _	20	. Depth Bridg	e Plug Set:	MD		
18. Total Depth:	TVD	6060	1 19.	Plug back	1.D.:	TVD		6062	C.		(Requires	Prior Approva	) TVD		
21. Type Electric &	other Logs Run (Su	ibmit 1 copy and 1	1 LAS of each),	Cased and	Open Hole,	Btm Hole Pres	s Survey			22. W	as well cored?	X	No	Yes (Sub	mit analysis)
			CEMEN	T, TVI	O, MD					W	as DST run?	X	No	Yes (Sub	mit report)
										Di	rectional Survey	?	No	X Yes (Sub	mit copy, w/ cert.)
23. Casing ar	d Liner Record	Report all strin	ngs set in well)							N. COL	0.77. 6				
Hole Size	Size/ Grade	Wt.	. (#/ft.)	Тор (	(MD)	Bottom(	MD)	Stage Cementer	Depth	200	. & Type of ment	Slurry Vol.	(Bbl) (	Cement Top*	Amount Pulled
13.5"	10.75"J-5		0.5#	0		176					10	445		0	
8.75"	5.5" P-110	0 2	20#	0		1094	15'			1:	500	1162	3	3900	
		_											_		
24. Tubing		(A (D)	D. I. D.	L () (D)		0'		epth Set (MD)	Deales	Donal (MD)	T 6:		David Cat	0.4D) I I	Dealer Death (MD)
Size 2 7/8"	Depth Se 586		Packer Dept			Size	Di	eptn Set (MD)	Packer	Depth (MD)	Siz	ze	Depth Set	(MD)	Packer Depth (MD)
	ng Intervals						26.	Perforation Rec	cord						
	Formation TELA DOG			op		Bottom	1	Perforated Inter	-		Size 1/8"	No. of Ho	oles		Status
A) B) B) B) B) B) B)	TEAPOT		66	75'	10	)795'		0643'- 1079 0395'- 1054			1/8"	32	+		TIVE TIVE
B)			_					0147'- 1029			1/8"	32			TIVE
B)								9898'- 1005			3 1/8"	32			TIVE
В)							1	9651'- 9803			3 1/8"	32			ΓΙVΕ
B)								9403'- 9555			3 1/8"	32			ΓΙVE
				-				9115'- 9307 8907'- 9061			3 1/8" 3 1/8"	32	-		TIVE TIVE
B)								8660'- 8811			3 1/8"	32	+		TIVE
B) B)			_					8411'- 8558			3 1/8"	32	_		TIVE
B)								8163'- 8315			3 1/8"	32			TIVE
В)							- 11	7915'- 8067			3 1/8"	32			TIVE
B)								7669'- 7819			3 1/8"	32			TIVE
B)								7419'- 7565 7171'- 7323			3 1/8" 3 1/8"	32	-		TIVE
B) B)			+				-	6923'- 7075			3 1/8"	32			TIVE TIVE
C)			_					6675'- 6827			3 1/8"	32	+		TIVE
D)															
	mary:	Tot	al Frac Stag	es:	17	Total Slur	ry (bbls)	:			Proppant (l				,546,040
28. Product Date First Produced	ion- Interval A		25. For		TEA Production	АРОТ Оіі вы		Gas MCF	Product Water Bbl	tive Interva	l: vity Corr. API	6675' -		795' Flowback Disp	oral
	Test Date		Hours Tested	Test	roduction			169	100		40		38893		
4/28/2015 Choke Size	Tbg.Press Fly	/2015 wg.	Csg Press.	24 H	r. Rate	Oil Bbl	76	Gas MCF	Water Bb			Res. Pre		Well Status	7,916
64/64	PSI	315	150	-	Ottombron of	4	76	169	100		356		,727	PRO	DUCING

29. Disposition of Gas (50)		a, etc.)		Test Witness	:					
30. Summary of Porous Zon	SOLD					31. Formation (Log) Markers:				
						3 22				
Show all important zones of time tool open, flowing and			ervals and all drill-stem tests,	including depth interval tested	d, cushion used	TEAPOT				
Formation TEAPOT	Top 6554'	Bottom 10795'	Descr OIL-GAS-WAT	iptions Contents, Etc.		Name FOX HILLS	TVD 4642			
						LEWIS TECKLA TEAPOT	4817 5554 6097			
32. Additional remarks; inc	clude plugging proced	ure (Req. prio	r approval):							
				LE 37-70-3-2 SWD / 1,082 IN	NTO REIHLE	37-70-3-3 SWD				
33. Indicate which items ha	ve been attached by pl	acing a check	in the appropriate boxes							
X Electrical/ Mechanica		& Open hole.		Geologic Report  Core Analysis		DST Report X Directional Press. Survey X Other:	Survey w/ Certification PLAT, FORM 10, CEMENT, BHL,			
			L_				CAS			
34. I hereby certify that the	foregoing and attache	ed information	is complete and correct	as determined from all av	ailable recore	ds (see attached instructions)*				
Name (please print)	HEATHER BI	REHM			Title	REGULATORY ANALYST				
Signature					Date					

### INSTRUCTIONS

If not filed prior to the time this summary record is submitted, copies of all currently available logs (drillers, geologists, sample and core analysis, all types electric, etc.), formation and pressure tests, and directional surveys should be attached hereto, to the extent required by applicable Federal and or State laws and regulations. All attachments should be listed on this form, see space 33.

Space 4: If there are no applicable State requirements, locations on Federal or Indian land should be described in accordance with Federal requirements. Please note all Lat./ Longs. In NAD 83. Calculate all "Top of Producing Intervals" and "BHL" first as distance from the section corner, second as the Lat. /Long. Spacing orders are based on a well location in a section. Well locations must match the surveyed footages.

Space 17: Indicate elevation used for depth measurements given in other spaces on this form and in any attachments.

Space 23: "Sacks Cement": Attached supplemental records for this well should show the details of any multiple stage cementing and the location of the cementing tool. Show how reported top(s) of cement were determined, i.e. circulated (CIR), or calculated (CAL), or cement bond log (CBL), or temperature survey (TS).

Spaces 25 and 28: If this well is completed for commingled production from more than one pool (multiple zone completion), state in space 25 and 26, and in space 25 show the producing interval, or intervals, top(s), bottom(s) and name(s) (if any) for the pools reported in space 28 through 28c. Submit a separate completion report on this form for each pool separately produced, (not commingled).

Space 27: If a well was fracture treated or stimulated, all data required in Chapter 3, Section 45 must be filed with this Completion Report.

### Space 27: If a well was fracture treated or stimulated, provide Summary Data for # of Stages, Total Slurry, Total Proppant

- Space 28: Provide well test data for each interval tested or stimulated and flowed.
- Space 32: Provide frac flowback disposal volumes and handling and disposal site.
- Space 32: Provide final annulus casing pressure.
- Space 32 or Attachment: Provide all Stimulation Chemicals by Name, Type, Volumes and CAS #s.

Attach a wellbore diagram whenever possible.

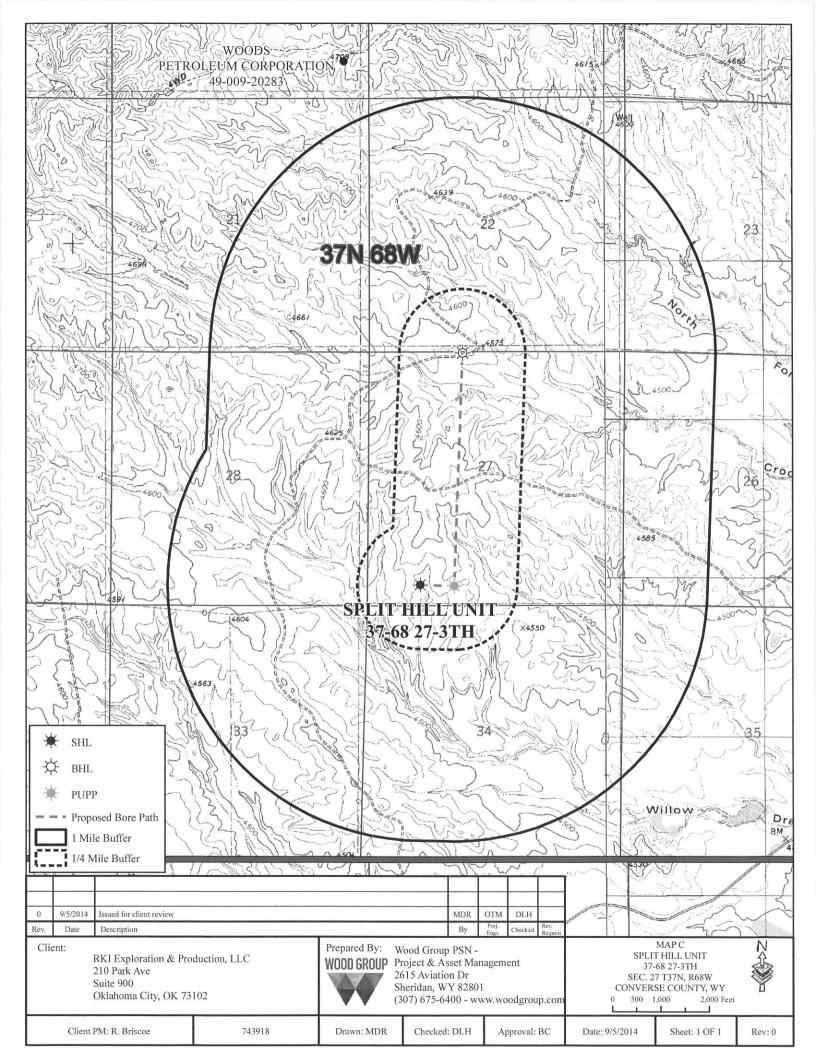
Form 10 DECEMBER, 2000 STATE OF WYOMING

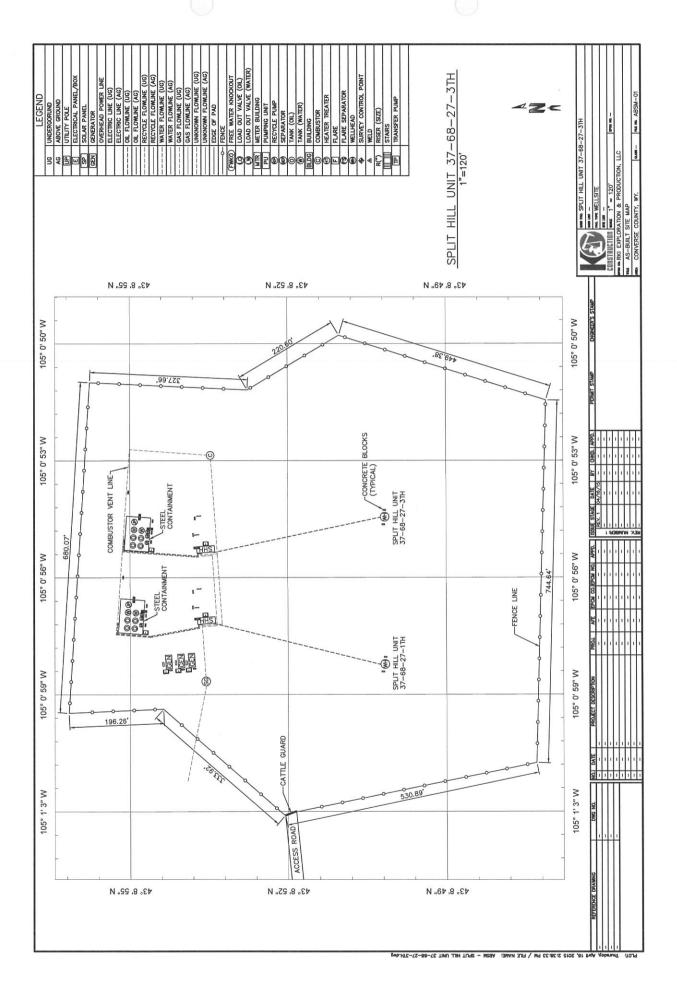
### OIL AND GAS CONSERVATION COMMISSION

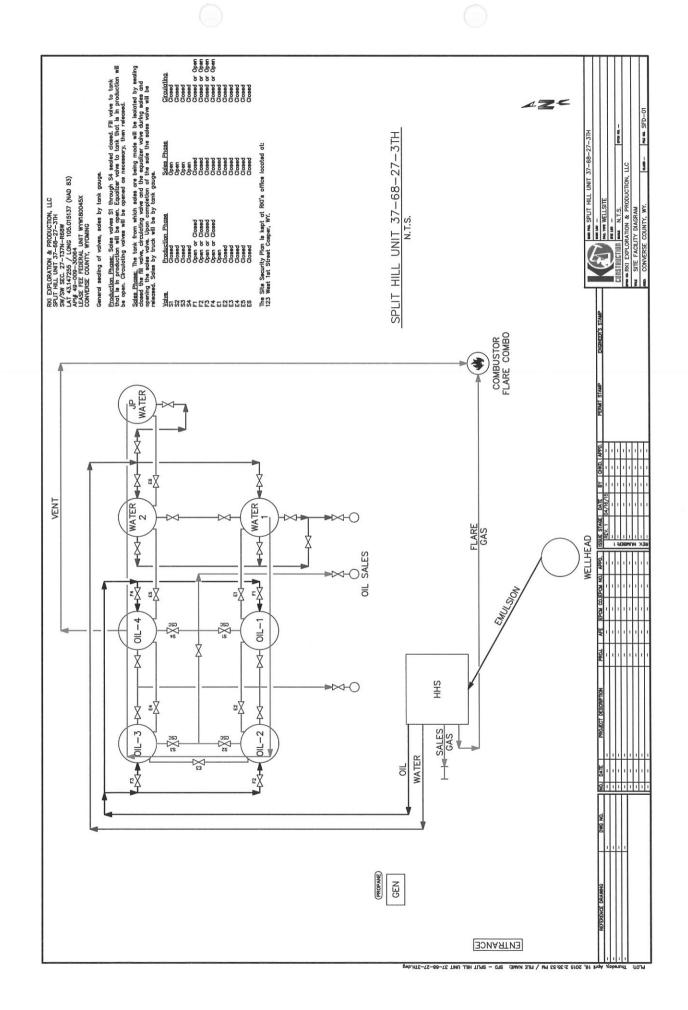
Office of State Oil and Gas Supervisor P.O. Box 2640

			30x 2640 yoming 826(	)2			
	PRODUCTI	ON TEST AND			REPORT	1	
OPERATOR					API NUMBER		
RKI EXPLORATION AND P	RODUCTION				49-009-30064	1	
ADDRESS	ROBUCTION				WELL NAME &		
210 PARK AVE., SUITE 900 OKLAHOMA CITY, OK 73012					SPLIT HILL U	NIT 37-68 27-3TH	ſ
LEASE NAME	RES	SERVOIR			FIELD		
SPLIT HILL UNIT		TE	APOT			WILDCAT	
LOCATION,(quarter-quarter and foo	tages): LATITUDE		LONGITUDE:	-105.015137°	COUNTY	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,	
SW/SW 350' FSL	1,275' FWL	Sec. 27 , Twp.	37 N ,	Rge. 68 W		CONVER	RSE
		TEST	DATA				
START OF TEST-DATE	TIME	END OF TEST-DATE		TIME	DURATION OF	TEST	
5/5/2015	3:00 PM	5/6/2015		3:00 PM		24 HRS	
	CASING PRESSURE		ESSURE	SEPARATOR TI	EMP.	CHOKE SIZE	
315	150	10	00	11	0°F	64/6	54
OIL PRODUCTION DURING TEST		GAS PRODUCTION DURI				UCTION DURING TI	14(4)
486.86		1.60.00			1.0	00.27	
476.76 OIL GRAVITY	bbls.	PRODUCING METHOD (I	Flowing numni	MCF	1,00	08.36 bt	bls.
OLL GRAVIII		TRODUCTION (I	lowing, pumpi	ing, gas int, etc.)			
40 *api				ESP			
		GAS PRO	DUCTI				
METER MANUFACTURER					ORIFICE WELL	TESTER	X
METER MANOTACTORER					ORIFICE WEEL	TESTER	A
TOTAL FLOW	Flange Tap	X PIPE TAP	L-10		CRITICAL FLO	W PROVER	
ORIFICE DIAMETER		PIPE DIAMETER (Inside d	ia.)		ORIFICE DIAM	ETER	
1			2.067			1	
DIFFERENTIAL PRESSURE RANC	Æ	MAX. STATIC PRESSURI	E RANGE		PIPE DIAMETE	R	
0-400			0-1500			2	
GAS GRAVITY (Air-1.0)		FLOWING, TEMPERATUR	Æ		GAS GRAVITY	(Air-1.0)	
0.88893 Meas. X			77°F		0.88893	Meas.	
0.88893 Meas. X DIFFERENTIAL NO FLOW READI	Est	STATIC NO FLOW READ			24 HOUR COEF		Est
	110	1			24 HOUR COLI		
-0.001 DIFFERENTIAL		STATIC	12.504		PRESSURE:	N/A (Indicate Units	(3)
21			26			PSIG	,
21		TEST I	RESULT	rs		1510	
DAILY OIL	DAILY WATER		DAILY GAS		GAS- OIL R	RATIO	
477 bbls.	1,00	8 bbls.	16	59.9 мс	F	356.36	SCF/STB
I hereby, swear or affirm that	the statements herei	in made are complete and	correct, ancl t	that the test describ	ed was made in a	accordance with the	)
rules, regulations and Instruc	tions of the Wyomin	ng Oil and Gas Conservati	on Commissi	on. SIGNATURE	Ad	andoh	_
				TITLE	SR. PRODU	UCTION ENGIN	EER
				DATE		5/14/2015	
SUBMIT I COPY ONLY				-		U, I 1/2013	

110	11/	Sol		22	23	1	19	20	21	22
		ed Facilities	28 <b>2</b> 1	27 :N-68\	26´ _	25	30	29	28	eld Road
*** > ***		551)Ft. 0 Rods	33	34	35	36	3.1	32	33	
) P	roposed Well P		-4	3	2		6	5 (	4	10000
	12,247 ft - 742.2/Rods	~ S M	9.	10. =	11-15	12	7	8		行い記録
15 - 14 37N 6	13 9W	18 17	16 <b>37N</b>	15 68VM://	14/	13	18	177 27N 671	16	12 00
22]=   23	-24-	19. 20	21	22 Proposed Access		24	19 Walker	20 Creek Ro	21 ad	
27 26	25	30 29 SPLIT I	28 <sup>-1</sup> HILL UNIT <b>27-1-3 T.H</b>	2,247 ft -	742.2 Ro 26	ds) 25	30	29	28	7
34 35	36	31 32	33	34	35	36 7	31.	32	33 33 ***	Comment of the last of the las
3 2 2,		6 5	4	3	2	1-5	6	5	4	
10 11	12	7 8	9	10	11.1	12		8	9 1	
36N-6	13 QW	182 17	16 <b>36N</b>	68W	14:*	13	18	17 20162	/16	7 7 5 7
1 22 23	24 <sup>+</sup> or	19 20	21	22	23	24	119	20	2-1	
. Leave Douglas, W		Priving Direc		tales 11 7 miles			₩ Well	Location		
2. Turn east onto Wal 3. Turn west onto pro	ker Creek road for a	pproximately 30.9	miles.					osed Acces ting Access		88
9/5/2014 Issued to clic	ent for review.			J.		DLH BC	Cour Well	nty Road Pad		
210 Park A Suite 900	ration & Production, L ve City, OK 73102	LC	Prepared By: WOOD GROUP	Wood Group P Project & Asset 2615 Aviation I Sheridan, WY 8 (307) 675-6400	SN - t Management Or 32801		SPL 37- SEC 2	CCESS MAP IT HILL UNIT -68 27-1,3TH 27, T37N, R68W RSE COUNTY, WY 6,000	7 12,000 Feet	1
Land Agent: R. Bris	coe	743918	Drawn: JDB	Checked: D	LH Appro	oval: BC	9/5/2014	Sheet: 1 OF 1	Rev	: 0



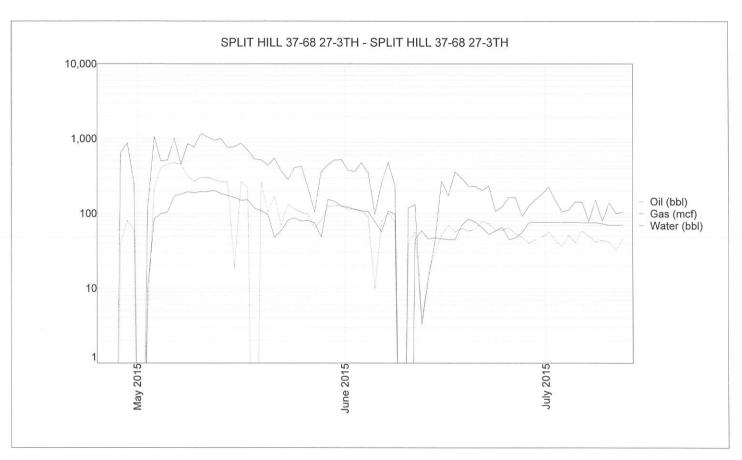






### Daily Production Report Time: 7/13/2015 SPLIT HILL 37-68 27-3TH - SPLIT HILL 37-68 27-3TH

Selected Time Frame: 06/13/2015 - 07/13/2015



Daily Braduation				Notes
Daily Production Date	Oil	Gas	Water	<dt> = Down Time <gm> = Gas Meter</gm></dt>
07/13/2015	0	ouo	vato:	Cas motor
07/12/2015	46.68	70	105.00	
07/11/2015	31.67	69	100.02	
07/10/2015	41.68	69	138.33	
07/09/2015	43.76	73	80.00	
07/08/2015	41.68	75	151.67	
07/07/2015	50.01	75	78.32	
07/06/2015	58.35	75	141.67	
07/05/2015	40.84	77	143.34	
07/04/2015	51.26	76	111.66	
07/03/2015	36.67	76	104.99	
07/02/2015	43.34	76	148.34	
07/01/2015	56.68	76	223.33	
06/30/2015	48.34	76	181.68	
06/29/2015	45.01	76	153.34	
06/28/2015	40.01	76	125.00	
06/27/2015	48.34	56	91.66	
06/26/2015	53.34	47	161.67	
06/25/2015	65.01	45	165.01	
06/24/2015	60.01	65	123.30	
06/23/2015	60.01	58	106.69	



### Daily Production Report Date: 7/13/2015 Time: 7:46 AM SPLIT HILL 37-68 27-3TH - SPLIT HILL 37-68 27-3TH

Selected Time Frame: 06/13/2015 - 07/13/2015

Daily Production Date	Oil	Gas	Water	Notes <dt> = Down Time <gm> = Gas Meter</gm></dt>
06/22/2015	73.35	52	233.33	
06/21/2015	77.93	65	203.32	
06/20/2015	61.68	77	229.99	
06/19/2015	58.35	85	233.33	
06/18/2015	63.35	70	296.68	
06/17/2015	56.68	45	360.02	
06/16/2015	69.60	45	173.32	<dt> NA, Production coming up after 20 hour run time</dt>
06/15/2015	51.68	46	270.00	<dt> Jet Pump Failure, Love joy melted replaced with new hubs back online at 530 pm</dt>
06/14/2015	30.01	47	43.34	<dt> Jet Pump Failure, Went down on high vibration replaced Vibration Murphry switch</dt>
06/13/2015	16.67	46	13.34	<dt> Jet Pump Failure, Love joy melted got it replaced and running at 4:45PM</dt>
Total:	1,521.97	1,966	4,691.69	Construction of the constr
Average:	50.73	66	156.39	

RKI Exploration & Production, LLC Split Hill 37-68-27 PAD 3TH (Teapot Formation) sw sw 27-37N-68W Converse County, Wyoming

## Heater Treater (HTR01)

Run time (hrs): 8,760

Burner Size: 0.500 MMBtu/hr

Fuel Heat Value: 1,

1,020 btu/scf

-		
	N20	0.00
	Methane	0.00
	C02	257.65
	HAPs	00'0
otential Emissions (tpy)	H2S	00.00
Potential En	PM10	0.02
	802	00:00
	VOC	0.01
	00	0.18
	NOx	0.21
		HTR-1

					Potential Emi	otential Emissions (lb/hr)				
	NOx	00	VOC	202	PM10	H2S	HAPs	C02	Methane	N20
HTR-1	0.049	0.041	0.001	00.00	0.004	0.000	0.000	58.8235294	58.8235294 0.00112745 0.00107843	0.00107843

Emission Factors (AP42 1.4 - Natural Gas Combustion)

	lb/MMscf	lb/MMscf   lb/MMBtu	
NOx	100	0.09803922	AP-42 Table 1.4-1
00	84	0.08235294	AP-42 Table 1.4-1
VOC	5.5	0.00539216	AP-42 Table 1.4-2
PM	9.7	0.00745098	AP-42 Table 1.4-2
502	09:0	0.00058824	AP-42 Table 1.4-2
CO2	120000	117.647059	AP-42 Table 1.4-2
Methane	2.3	0.0022549	AP-42 Table 1.4-2
N2O	2.2	0.00215686	AP-42 Table 1.4-2

```
*******************************
* Project Setup Information
******************************
          : M:\Users\JIngerson\Wyoming Air Applications\Split Hill 37-68-27 PAD\Split Hill
Project File
Flowsheet Selection : Oil Tank with Separator Calculation Method : RVP Distillation Control Efficiency : 98.0%
Known Separator Stream : Low Pressure Oil
Entering Air Composition : No
Filed Name
                 : Powder River Basin, Wyoming
Well Name
                 : Split Hill 37-68-27 3TH Oil
Well ID
                  : 49-009-30064
Date
                  : 2015.07.13
****************************
* Data Input
********************
Separator Pressure
                 : 85.00[psig]
Separator Temperature : 100.00[F]
Ambient Pressure
                  : 12.50[psia]
Ambient Temperature
                 : 55.00[F]
C10+ SG
                 : 0.80927
                 : 227.567
C10+ MW
-- Low Pressure Oil ------
  No.
     Component
  1
      H2S
                      0.0000
  2
       02
                      0.0000
  3
      CO2
                      0.0640
      N2
                      0.0130
      C1
  5
                      0.6320
      C2
  6
                      0.1430
  7
      C3
                      0.8760
  8
      i-C4
                      0.9670
  9
      n-C4
                      2.5800
  10
      i-C5
                      1.4320
  11
      n-C5
                      1.8450
  12
      C6
                      1.6680
  13
      C7
                      6.4210
  14
      C8
                     16.5700
  15
       C9
                     11.7380
      C10+
  16
                     51.0870
  17
      Benzene
                     0.1240
                      0.4620
  18
      Toluene
  19
      E-Benzene
                      0.1390
      Xylenes
  20
                      1.6590
  21
      n-C6
                      1.2780
  22
      224Trimethylp
                      0.3020
-- Sales Oil ------
Production Rate : 31[bbl/day]
Days of Annual Operation : 365 [days/year]
API Gravity : 40.7
Reid Vapor Pressure
                 : 6.80[psia]
*************************
   Calculation Results
***********************************
-- Emission Summary ------
Item
              Uncontrolled Uncontrolled Controlled Controlled
              [ton/yr]
                        [lb/hr]
                               [ton/yr]
                                             [lb/hr]
```

Total HC 1 VOCs, C2+ 0	0.010 1.076 0.601 0.543	0.002 0.246 0.137 0.124	0.00 0.02 0.01 0.01	2 2	0.000 0.005 0.003 0.002		
	T 6						
Uncontrolled Recovery Vapor	y info. 90.4400 x1E-3	[MSCFD]					
	85.4600 x1E-3						
GOR 2	2.92	[SCF/bbl]					
Emission Compositi	ion Uncontrolled	Uncontrol		rolled	Controlle		
territoria de la compania del compania de la compania del compania de la compania del la compania de la compani	[ton/yr]	[lb/hr]		/yr]	[lb/hr]	u.	
	0.000	0.000	0.00		0.000		
2 02 0	0.000	0.000	0.00	0	0.000		
	0.064	0.015	0.06		0.015		
	0.027	0.006	0.02		0.006		
	0.476 0.058	0.109 0.013	0.01		0.002		
	0.159	0.036	0.00		0.001		
	0.088	0.020	0.00		0.000		
	0.164	0.037	0.00		0.001		
	0.041	0.009	0.00		0.000		
	0.038 0.011	0.009 0.003	0.00		0.000		
	0.016	0.004	0.00		0.000		
	0.014	0.003	0.00		0.000		
	0.003	0.001	0.00		0.000		
	0.000	0.000	0.00		0.000		
	0.001 0.001	0.000	0.00		0.000		
	0.000	0.000	0.00		0.000		
	0.001	0.000	0.00		0.000		
	0.007	0.002	0.00		0.000		
	0.001	0.000	0.00		0.000		
Total 1	1.170	0.267	0.02	.3	0.005		
Stream Data							
No. Component	MW	LP Oil		Sale Oil			Total Emissions
1 1129	24 00	mol %	mol %	mol %	mol %	mol %	mol %
1 H2S 2 O2	34.80 32.00	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000 0.0000
3 CO2	44.01	0.0640	0.0492	0.0492	3.3146	0.0000	3.3146
4 N2	28.01	0.0130	0.0031	0.0031	2.1969	0.0000	2.1969
5 C1	16.04	0.6320	0.3256	0.3256	68.0697	0.0000	68.0697
6 C2	30.07	0.1430	0.1236	0.1236	4.4100	0.0000	4.4100
7 C3 8 i-C4	44.10 58.12	0.8760 0.9670	0.8423 0.9556	0.8423	8.2887 3.4831	0.0000	8.2887 3.4831
9 n-C4	58.12	2.5800	2.5624	2.5624	6.4615	0.0000	6.4615
10 i-C5	72.15	1.4320	1.4326	1.4326	1.2957	0.0000	1.2957
11 n-C5	72.15	1.8450	1.8478	1.8478	1.2181	0.0000	1.2181
12 C6	86.16	1.6680	1.6742	1.6742	0.3049	0.0000	0.3049
13 C7 14 C8	100.20 114.23	6.4210 16.5700	6.4485 16.6440	6.4485 16.6440	0.3678 0.2812	0.0000	0.3678 0.2812
15 C9	128.28	11.7380	11.7910	11.7910	0.0648	0.0000	0.0648
16 C10+	227.57	51.0870	51.3191	51.3191	0.0001	0.0000	0.0001
17 Benzene	78.11	0.1240	0.1245	0.1245	0.0167	0.0000	0.0167
18 Toluene	92.13	0.4620	0.4640	0.4640	0.0163	0.0000	0.0163
<pre>19 E-Benzene 20 Xylenes</pre>	106.17 106.17	0.1390 1.6590	0.1396 1.6665	0.1396 1.6665	0.0015 0.0156	0.0000	0.0015 0.0156
21 n-C6	86.18	1.0390	1.2830	1.2830	0.1793	0.0000	0.1793
22 224Trimethylp	114.24	0.3020	0.3033	0.3033	0.0136	0.0000	0.0136
		1.05 0-		100 1:	06.70	0.00	06.80
MW Stream Mole Ratio	0	165.80	166.44 0.9955	166.44 0.9955	26.79 0.0045	0.00	26.79
Heating Value	o [BTU/SCF]	1.0000	0.9933	0.3333	1466.18	0.000	0.0045 1466.18
Gas Gravity	[Gas/Air]				0.92	0.00	0.92
Bubble Pt. @ 1001	F [psia]	27.79	17.03	17.03			

RVP @ 100F [psia] 7.63 6.24 6.24 Spec. Gravity @ 100F 0.705 0.705

```
************************
   Project Setup Information
******************************
Calculation Method : RVP Distillation
Control Efficiency : 98 02
Known Server
          : M:\Users\JIngerson\Wyoming Air Applications\Split Hill 37-68-27 PAD\Split Hill
Known Separator Stream : Low Pressure Oil
Entering Air Composition : No
Filed Name
                 : Powder River Basin, Wyoming
Well Name
                 : Split Hill 37-68-27 3TH Water @ 1% Oil
Well ID
                 : 49-009-30064
Date
                 : 2015.07.13
***********************
* Data Input
*******************
Separator Pressure
                : 85.00[psig]
Separator Temperature : 100.00[F]
Ambient Pressure
                 : 12.50[psia]
Ambient Temperature
                 : 55.00[F]
C10+ SG
                : 0.80927
C10+ MW
                 : 227.567
-- Low Pressure Oil ------
  No.
     Component
  1
      H2S
                     0.0000
  2
      02
                     0.0000
  3
      CO2
                     0.0640
                     0.0130
      N2
      C1
                     0.6320
  5
      C2
  6
                     0.1430
  7
      C3
                     0.8760
  8
      i-C4
                     0.9670
  9
      n-C4
                     2.5800
  10
      i-C5
                     1.4320
  11
      n-C5
                     1.8450
  12
      C6
                     1.6680
  13
      C7
                     6.4210
  14
      C8
                     16.5700
  15
      C9
                     11.7380
      C10+
  16
                    51.0870
  17
      Benzene
                     0.1240
                     0.4620
  18
      Toluene
  19
      E-Benzene
                     0.1390
      Xylenes
  20
                     1.6590
  21
      n-C6
                     1.2780
  22
      224Trimethylp
                     0.3020
-- Sales Oil ------
Production Rate : 1[bbl/day]
Days of Annual Operation : 365 [days/year]
API Gravity : 40.7
Reid Vapor Pressure
                 : 6.80[psia]
*************************
* Calculation Results
*******************************
-- Emission Summary ------
Item
             Uncontrolled Uncontrolled Controlled Controlled
             [ton/yr]
                       [lb/hr]
                              [ton/yr]
                                            [lb/hr]
```

Total HAPs

0.000 0.000 0.000 0.000

	al naps	0.000	0.000	0.00		0.000		
	al HC	0.035	0.008	0.00		0.000		
VOC	s, C2+	0.019	0.004	0.00	0	0.000		
VOC	s, C3+	0.018	0.004	0.00	0	0.000		
	-,		5,5,5,5,5		-			
Unc	ontrolled Recove:	ry Info.						
	Vapor	2.9200 x1E-3	[MSCFD]					
	HC Vapor	2.7600 x1E-3	[MSCFD]					
	GOR	2.92	[SCF/bbl]					
	Emission Composi	tion						
No	Component	Uncontrolled		led Cont	rolled	Controlle	d	
110	component						<b>u</b>	
		[ton/yr]	[lb/hr]	[ton		[lb/hr]		
1	H2S	0.000	0.000	0.00	0	0.000		
2	02	0.000	0.000	0.00	0	0.000		
3	CO2	0.002	0.000	0.00		0.000		
4	N2	0.001	0.000	0.00	1	0.000		
5	C1	0.015	0.003	0.00	0	0.000		
6	C2	0.002	0.000	0.00	0	0.000		
7	C3	0.005	0.001	0.00		0.000		
8	i-C4	0.003	0.001	0.00	0	0.000		
9	n-C4	0.005	0.001	0.00	0	0.000		
10	i-C5	0.001	0.000	0.00	0	0.000		
11	n-C5	0.001	0.000	0.00		0.000		
12	C6	0.000	0.000	0.00		0.000		
13	C7	0.001	0.000	0.00	0	0.000		
14	C8	0.000	0.000	0.00	0	0.000		
15	C9	0.000	0.000	0.00		0.000		
16	C10+	0.000	0.000	0.00		0.000		
17	Benzene	0.000	0.000	0.00	0	0.000		
18	Toluene	0.000	0.000	0.00	0	0.000		
19		0.000	0.000	0.00		0.000		
20	Xylenes	0.000	0.000	0.00		0.000		
21	n-C6	0.000	0.000	0.00	0	0.000		
22	224Trimethylp	0.000	0.000	0.00	0	0.000		
	Total	0.036	0.008	0.00		0 000		
	Total	0.036	0.008	0.00		0.000		
			0.008	0.00		0.000		
	Total Stream Data		0.008	0.00		0.000		
			0.008  LP Oil		1	0.000  Flash Gas		 Total Emissions
	Stream Data		LP Oil	 Flash Oil	1  Sale Oil	 Flash Gas		
No.	Stream Data Component	MW	LP Oil	Flash Oil	Sale Oil	Flash Gas	mol %	mol %
No.	Stream Data Component H2S	 МW 34.80	LP Oil mol % 0.0000	Flash Oil mol % 0.0000	1  Sale Oil mol % 0.0000	Flash Gas mol % 0.0000	mol % 0.0000	mol % 0.0000
No. 1 2	Stream Data Component H2S O2	MW 34.80 32.00	LP Oil mol % 0.0000 0.0000	Flash Oil mol % 0.0000 0.0000	Sale Oil mol % 0.0000 0.0000	Flash Gas mol % 0.0000 0.0000	mol % 0.0000 0.0000	mol % 0.0000 0.0000
No.	Stream Data Component H2S	 МW 34.80	LP Oil mol % 0.0000	Flash Oil mol % 0.0000	1 Sale Oil mol % 0.0000	Flash Gas mol % 0.0000	mol % 0.0000	mol % 0.0000
No. 1 2	Stream Data Component H2S O2	MW 34.80 32.00	LP Oil mol % 0.0000 0.0000	Flash Oil mol % 0.0000 0.0000	Sale Oil mol % 0.0000 0.0000	Flash Gas mol % 0.0000 0.0000	mol % 0.0000 0.0000	mol % 0.0000 0.0000
No.  1 2 3 4	Stream Data Component H2S O2 CO2 N2	MW 34.80 32.00 44.01 28.01	LP Oil mol % 0.0000 0.0000 0.0640 0.0130	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031	1 Sale Oil mol % 0.0000 0.0000 0.0492 0.0031	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969	mol % 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969
No.  1 2 3 4 5	Stream Data Component H2S O2 CO2 N2 C1	MW  34.80 32.00 44.01 28.01 16.04	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256	1 Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697	mol % 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697
No.  1 2 3 4 5	Stream Data Component  H2S 02 C02 N2 C1 C2	MW  34.80 32.00 44.01 28.01 16.04 30.07	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100	mol % 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100
No.  1 2 3 4 5 6 7	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697
No.  1 2 3 4 5	Stream Data Component  H2S 02 C02 N2 C1 C2	MW  34.80 32.00 44.01 28.01 16.04 30.07	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100	mol % 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100
No.  1 2 3 4 5 6 7	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831
No.  1 2 3 4 5 6 7 8	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615
No.  1 2 3 4 5 6 7 8 9 10	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957
No.  1 2 3 4 5 6 7 8 9 10 11	Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478	Sale Oil mol % 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957
No.  1 2 3 4 5 6 7 8 9 10	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957
No.  1 2 3 4 5 6 7 8 9 10 11 12	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049
No.  1 2 3 4 5 6 7 8 9 10 11 12 13	Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167	mol % 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17	LP Oil mol % 0.0000 0.0040 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	Sale Oil mol % 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17	LP Oil mol % 0.0000 0.0040 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	Sale Oil mol % 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18	LP Oil mol % 0.0000 0.0040 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	LP Oil mol % 0.0000 0.0040 0.0130 0.6320 0.1430 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033 166.44	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp  MW Stream Mole Rat	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.00492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp  MW Stream Mole Rat Heating Value	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020 165.80 1.0000	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033 166.44	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136  26.79 0.0045 1466.18	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136  26.79 0.0045 1466.18
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp  MW Stream Mole Rat Heating Value Gas Gravity	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	LP Oil mol % 0.0000 0.00640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020 165.80 1.0000	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 1.6742 6.4485 1.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033 166.44 0.9955	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136
No.  1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 20 21	Stream Data Component  H2S O2 CO2 N2 C1 C2 C3 i-C4 n-C4 i-C5 n-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224Trimethylp  MW Stream Mole Rat Heating Value	MW  34.80 32.00 44.01 28.01 16.04 30.07 44.10 58.12 58.12 72.15 72.15 86.16 100.20 114.23 128.28 227.57 78.11 92.13 106.17 106.17 86.18 114.24	LP Oil mol % 0.0000 0.0000 0.0640 0.0130 0.6320 0.1430 0.8760 0.9670 2.5800 1.4320 1.8450 1.6680 6.4210 16.5700 11.7380 51.0870 0.1240 0.4620 0.1390 1.6590 1.2780 0.3020 165.80 1.0000	Flash Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033	Sale Oil mol % 0.0000 0.0000 0.0492 0.0031 0.3256 0.1236 0.8423 0.9556 2.5624 1.4326 1.8478 1.6742 6.4485 16.6440 11.7910 51.3191 0.1245 0.4640 0.1396 1.6665 1.2830 0.3033 166.44	Flash Gas mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136  26.79 0.0045 1466.18	mol % 0.0000	mol % 0.0000 0.0000 3.3146 2.1969 68.0697 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.2812 0.0648 0.0001 0.0167 0.0163 0.0015 0.0156 0.1793 0.0136  26.79 0.0045 1466.18

RVP @ 100F [psia] 7.63 6.24 6.24 Spec. Gravity @ 100F 0.705 0.705

Split Hill 37-68-27 PAD 3TH (Teapot Formation) RKI Exploration & Production, LLC sw sw 27-37N-68W Converse County, Wyoming

Oil Loadout

Model: OIL LOAD-1 Oil Truck Loadout Source ID Number: Name

Liquid Loading

469098 26.82 Molecular Weight (lb/lb-mole): Throughput Value (gal/yr): Liquid Temperature (°F): Vapor Pressure (psia)

0.6 365 60.00 Days Per Year: Load Duration (min/truck): Saturation Factor: 55 6.80 24 47

Hours Per Day: Load Frequency (trucks/yr):

Loading Loss (lb/1000 gal) = (12.46\*5\*P\*M)/T (AP-42 Section 5.2 (1/95)) where:

S = Saturation Factor = dedicated normal service

P = True Vapor Pressure of liquid loaded\*, psia

T = Temp. of bulk liquid loaded, deg. R = (deg. F + 460) M = Molecular Weight of Vapors, Ib/Ib-mole

Loading Loss (lb VOC/1000 gal) =

2.65 lb/1000 gal

### **Uncontrolled Emissions**

Pollutant	Loading Loss	Throughput		Estimated Emissions	Source of Emission Factor
	(lb/1000 gal)	(gal/yr)	(Ib/yr)	(tpy)	
VOC (includes HAPs)	2.65	469098	1241.92	0.62	AP42
			lb/hr: 0.1418		

### **Controlled Emissions**

.Uduliig LU33	IIIIougiibut			Emission Eactor
lb/1000 gal)	(gal/yr)	(lb/yr)	(tpy)	TO SECOND

0.0028 lb/hr:

## Split Hill 37-69-36 PAD 3TH (Teapot Formation)

Converse County, Wyoming 11/20/2014 jli ne nw 36-37N-69W

Water Loadout

Throughput Value assumes 1% oil in water volume. NOTE:

Model: WATER LOAD-1 Source ID Number: Name

Liquid Loading Water Truck Loadout 15330 0.6 365 60.00 26.82 Molecular Weight (lb/lb-mole): Throughput Value (gal/yr): Days Per Year: Load Duration (min/truck): Saturation Factor: 55 6.80 24 2 Load Frequency (trucks/yr): Liquid Temperature (°F): Vapor Pressure (psia) Hours Per Day:

Loading Loss (lb/1000 gal) = (12.46\*5\*P\*M)/T (AP-42 Section 5.2 (1/95)) where:

S = Saturation Factor = dedicated normal service

P = True Vapor Pressure of liquid loaded\*, psia

M = Molecular Weight of Vapors, 1b/1b-mole

T = Temp. of bulk liquid loaded, deg. R = (deg. F + 460)

2.65 lb/1000 gal Loading Loss (lb VOC/1000 gal) =

## **Uncontrolled Emissions**

Pollutant	Loading Loss	Throughput	Est	stimated Emissions	Source of Emission Factor
	(lb/1000 gal)	(gal/yr)	(lb/yr)	(tpy)	
VOC (includes HAPs)	2.65	15330	40.59	0.02	AP42
			lb/hr: 0.0046		

**Estimated Emissions** Loading Loss Throughput Controlled Emissions Pollutant

Pollutant	Loading Loss	Throughput	Estin	Estimated Emissions	Source of Emission Factor
	(lb/1000 gal)	(gal/yr)	(lb/yr)	(tpy)	
VOC (includes HAPs)	0.05	15330	0.81	0.00	Combustor Specs

0.0001

lb/hr:

Split Hill 37-68-27 PAD 3TH (Teapot Formation) RKI Exploration & Production, LLC sw sw 27-37N-68W Converse County, Wyoming

## Fugitive Emissions (3TH FUG-1)

**Uncontrolled Emissions** 

**100.00** Per AMR Gas Analysis of 6/9/2014 **94.79** Per AMR Gas Analysis of 6/9/2014 **40.45** Per AMR Gas Analysis of 6/9/2014 **1.29** Per AMR Gas Analysis of 6/9/2014

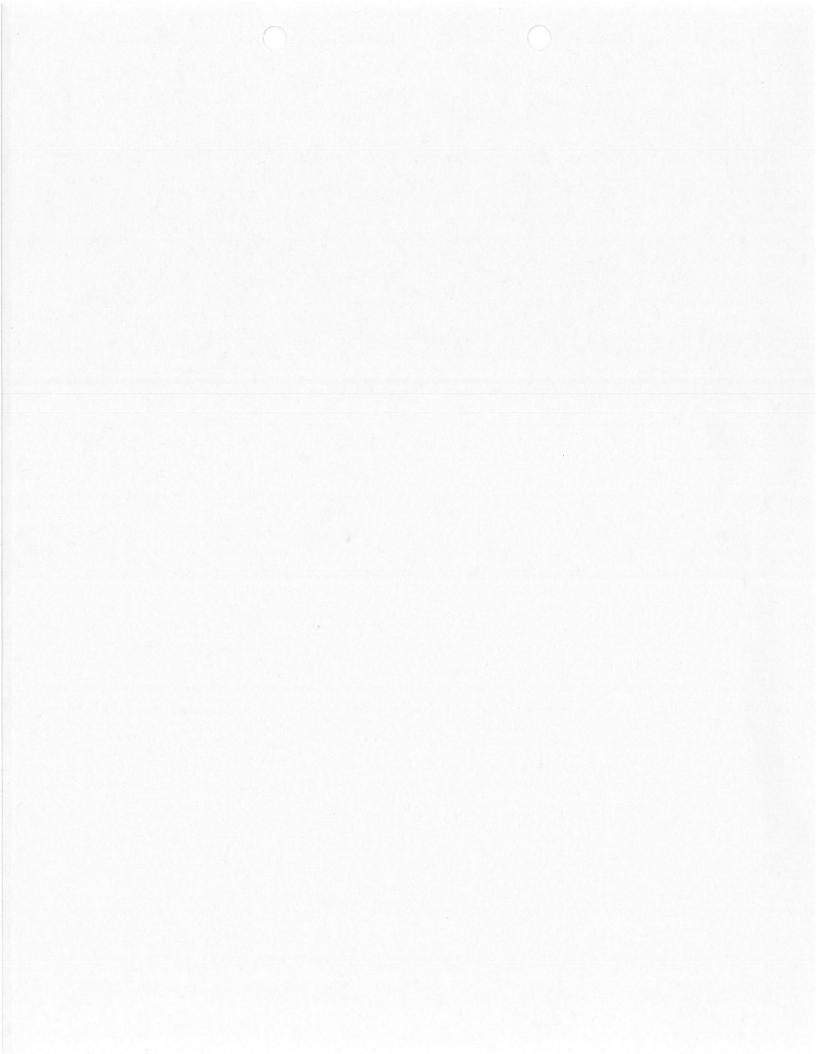
Wt Percent VOC: Wt Percent HAPs:

Wt Perecent Gas: Wt Percent HC:

									Leak Rate in Tons Per Year	ons Per Year	
Equipment Type	Gas Leak EF	Source	Percent	Percent	Percent	Operated	Gas Rate	Gas Rate	HC Rate	VOC Rate	HAPs Rate
	lb/hr/source	Count	HC	voc	HAPs	Hours	lb/hr	tpy	tpy	tpy	tpy
Valves	0.005420	75	94.79	40.45	1.29	8,760	0.3853	1.688	1.600	0.683	0.001
Flanges	0.000241	118	94.79	40.45	1.29	8,760	0.0270	0.118	0.112	0.048	0.000
Connectors	0.000458	124	94.79	40.45	1.29	8,760	0.0538	0.236	0.224	0.095	0.000
Other	0.016666	17	94.79	40.45	1.29	8,760	0.2686	1.176	1.115	0.476	0.001
Open Ended Lines	0.003080	-	94.79	40.45	1.29	8,760	1	1	1	1	1
Pumps	0.028750	1	94.79	40.45	1.29	8,760	-	1		1	1
Totals							0.735	3.218	3.050	1.302	0.002

Notes: See attached Gas Analysis for VOC and HAPs weight percent calculations.

Oil and Gas Production Operations leak emissions factors from EPA 453/R-95-017.



### **Control Equipment:**

### Flare/Combustor

Manufacturer:	Steffes		Date Install	ed:	4/28/2015
Model Name and	HP Flare		Company C	ontrol	
Number:	SHP-6		Equipment	ID:	FLR01
Company Control Equip	ment				
Description:		6" diameter	x 24' high H	P Flare Stac	k
Pollutant(s) Controlled:	CO  PM Condensible	NOx Pb	□ \$02 □ PM 2.	✓ VOC 5 (FIL)	☐ PM ☐ PM 2.5
✓ Other: <b>HAPs</b>					
Design Control Efficience Operating Control Effic		98 Capture Eff	ficiency (%):	,	100
Flare Type:	Elevated- Open	Elevated Fl	are Type:	Non-A	ssisted
Ignition Device:	Yes	Flame Presence Senso	r:	Yes	
Inlet Gas Temp (F):	100	Flame Pres	ence Type:		Thermocouple
Gas Flow Rate (acfm):	4	6.25	Outlet Gas	Temp (F):	1850
✓ This is the company that the comp	nly control equipmen	t on this air contaminan	t source		
If not, this control equi	oment is:	Primary	Seco	ndary	Parallel
List all other emission u	ınits that are also				
vented to this control e	quipment:	Heater Treater for 1T	H & 3TH un	til pipeline o	connection
List all release point IDs	associated with this				
control equipment:		Flare Stack 01			

**Emissions Information-** The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

FLR01 Used 876 hr/yr

			Effic	iency Standards	7		
		Pre-Controlled	Potential		Potential	Potential	T
		Potential Emissions	to Emit	_	to Emit	to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
teria Po	llutants:						
1.)					T		
	Particulate emissions						
	(PE/PM) (formerly						
	particulate matter,						
	PM)						
2.)						<u> </u>	
,	PM #10 microns in						
	diameter (PE/PM10)						
3.)							
3.,	PM #2.5 microns in						
	diameter (PE/PM2.5)						
4)	Sulfur dioxide (SO2)					-	
	Nitrogen Oxides	2.34	1		0.534	2.34	Other
5.,	(NOx)	2.5			0.554	2.54	other.
6.)	Carbon monoxide	0.585			0.134	0.585	Other
,	(CO)					0.000	
7.)	Volatile organic						
	compounds (VOC)						
8.)	Lead (Pb)						
	Total Hazrdous Air						
- 1	Pollutants (HAPs)						
10.)	Fluoride (F)						
	Hydrogen Sulfide						
100000000	(H2S)						
12.)	Mercury (Hg)						
	Total Reduced Sulfur						
,	(TRS)						
14.)	Sulfuric Acid Mist						
/	(SAM)						

<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

### Hazardous Air Pollutants (HAPs) and Toxic Air Contaminents

			Effic	iency Standards			
	I	Pre-Controlled	Potential		Potential	Potential	
	- 1	Potential Emissions	to Emit		to Emit	to Emit	Basis for
		tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:							
1.)							
2.)							
3.)							
4.)							
5.)							
6.)							
7.)							
8.)							

### Greenhouse Gases (GHGs)

				_		
		Efficier	ncy Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						***************************************
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

### **Control Equipment:**

### Flare/Combustor

Manufacturer:	Steffes		Date Install	ed:	4/28/2015
Model Name and	LP Flare	9	Company C	ontrol	
Number:	SVG-3		Equipment	ID:	FLR02
Company Control Equip	ment				
Description:		3" diamete	er x 24' high L	P Flare Stac	k
Pollutant(s) Controlled:  PM (FIL)  Other: HAPs	PM Condensib	NOx Pb	SO2 PM 2	<b>∨ vo</b> € 5 (FIL)	PM PM 2.5
Design Control Efficience	cy (%):	98 Capture E	Efficiency (%):		100
Operating Control Effici	ency (%):	98	<u> </u>		
Flare Type:	Elevated- Open	Elevated	Flare Type:	Non-A	ssisted
Ignition Device:	Yes	Flame Presence Sens	or:	Yes	
Inlet Gas Temp (F):	100	Flame Pro	esence Type:		Thermocouple
Gas Flow Rate (acfm):	Management	0.22	<b>Outlet Gas</b>	Temp (F):	1850
	30 00	nt on this air contamina			П
If not, this control equip		☐ Primary	□ Secor	ndary	Parallel
List all other emission u					
vented to this control e	quipment:	Oil & Water Tanks, L	oadout Facili	ties for 1TH	& 3TH
List all release point IDs	associated with this	5			
control equipment:		Flare Stack 02			

FLR02

**Emissions Information-** The following tables request information needed to determine the applicable requirements and the compliance status of this emission unit with those requirements.

	a			ency Standards			
		Pre-Controlled Potential Emissions	Potential to Emit		Potential to Emit	Potential to Emit	Basis for
		(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
iteria Po	llutants:						
1.)	Particulate emissions (PE/PM) (formerly particulate matter, PM)						
2.)							
3.)	PM #2.5 microns in diameter (PE/PM2.5)						5
4.)	Sulfur dioxide (SO2)						
5.)	Nitrogen Oxides (NOx)	0.012			0.003	0.012	Other
6.)	Carbon monoxide (CO)	0.003			0.001	0.003	Other
7.)	Volatile organic compounds (VOC)						
8.)	Lead (Pb)						
9.)	Total Hazrdous Air Pollutants (HAPs)						
10.)	Fluoride (F)						
11.)	Hydrogen Sulfide (H2S)						
12.)	Mercury (Hg)						
13.)	Total Reduced Sulfur (TRS)						
14.)	Sulfuric Acid Mist (SAM)						

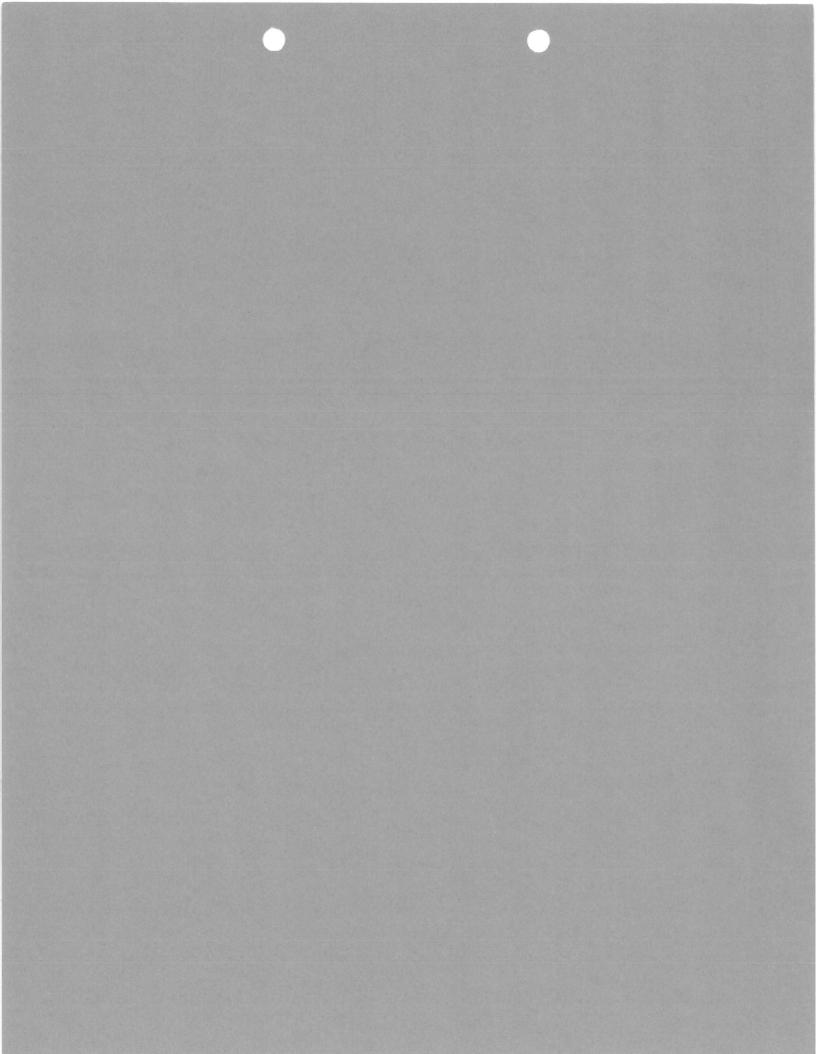
<sup>\*</sup>Provide your calculations as an attachment and explain how all process variables and emissions factors were selected.

### Hazardous Air Pollutants (HAPs) and Toxic Air Contaminents

		Effic	iency Standards	1		
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)					136.4	
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						

### Greenhouse Gases (GHGs)

		Efficie	ncy Standards			
	Pre-Controlled	Potential		Potential	Potential	
	Potential Emissions	to Emit		to Emit	to Emit	Basis for
	(tons/yr)	(PTE)	Units	(lbs/hr)	(tons/yr)	Determination
Pollutants:						
1.)						
2.)						
3.)						
4.)						
5.)						
6.)						
7.)						
8.)						



### **RKI Exploration & Production, LLC** Split Hill 37-69-36 PAD (Teapot Formation) ne nw 36-37N-69W **Converse County, Wyoming**

### **LP Production Flare (FLR-2)**

NOTE: Combined emissions for both 1TH and 3TH.

Flare Size:

106 mcfd nominal

Flare Size:

8 mmbtu/hr with 1748 btu/scf gas

**Operating Hours:** 

8,760 hrs

Gas BTU Value:

1,467 BTU/scf

Gas to Flare:

13 scf/hr (3.03 mcfd flash gas rate)

Gas to Flare:

0.114 mmscf/yr

Gas to Flare:

0.019 mmbtu/hr (3.03 mcfd flash gas rate)

Gas to Flare:

167 mmbtu/yr

### **EMISSIONS FACTORS per WDEQ Guidance Document**

NOx

0.140

lb/mmbtu

CO

0.035

lb/mmbtu

### CONTROLLED

	EF	EF	<b>Emissions</b>	
	<u>lb/mmbtu</u>	<u>lb/hr</u>	ton/yr	<u>Remarks</u>
NOx	0.140	0.003	0.012	WDEQ Guidance
CO	0.035	0.001	0.003	WDEQ Guidance

### **NOTES:**

Input Value

Calculated Value

### RKI Exploration & Production, LLC Split Hill 37-68-27 PAD (Teapot Formation) sw sw 27-37N-68W Converse County, Wyoming

### **HP Production Flare (FLR-1)**

NOTE: Combined emisions for both 1TH and 3TH.

Flare Size: 1,100 mcfd nominal

Flare Size: 64 mmbtu/hr with 1361 btu/scf gas

Operating Hours: 8,760 hrs
Gas BTU Value: 1,375 BTU/scf

Gas to Flare: 2,775 scf/hr (66 mcfd production rate)

Gas to Flare: 24.309 mmscf/yr

Gas to Flare: 3.816 mmbtu/hr (66 mcfd production rate)

Gas to Flare: 33,425 mmbtu/yr

### **EMISSIONS FACTORS per WDEQ Guidance Document**

**NO**x 0.140 lb/mmbtu **CO** 0.035 lb/mmbtu

.0

### CONTROLLED

	EF	EF	Emissions	
	<u>lb/mmbtu</u>	<u>lb/hr</u>	ton/yr	<u>Remarks</u>
NOx	0.140	0.534	2.340	WDEQ Guidance
СО	0.035	0.134	0.585	WDEQ Guidance

### **NOTES:**

Input Value

Calculated Value

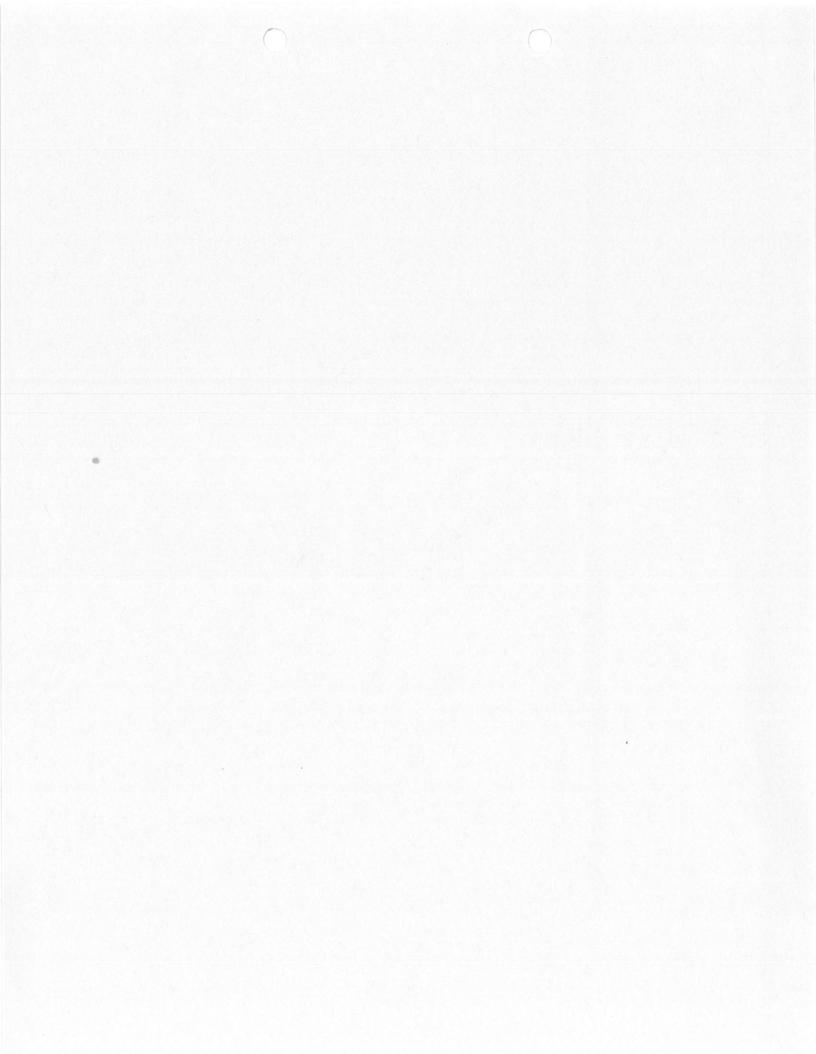
### **Release Point Information:**

Complete the table below for *each* release point. Please include release point information for each emission unit. Multiple attachments may be necessary. A release point is a point at which emissions from an emission unit are released into the ambient (outside)air. List each individual release point on a separate pair of lines (release point ID and description). *For longitude and latitude, use NAD 83/WGS84 datum and 5 digits after the decimal (i.e. 41.12345, -107.56789)* 

	Stack Release Point Information	
Company Release Point ID:	Release Point Type: Vertical	
FLR01	Release Point Latitude:	43.14725
	Release Point Longitude:	-105.01626
Company Release Point Description:	Base Elevation (ft):	4553
	Stack Height (ft):	24
<b>HP Heater Treater Flare</b>	Stack Diameter (ft):	0.5
	Exit Gas Velocity (ft/s):	1.82
	Exit Gas Temp (F):	1850
	Exit Gas Flow Rate (acfm):	51.4
Company Release Point ID:	Release Point Type: Vertical	
FLR02	Release Point Latitude:	43.14725
	Release Point Longitude:	-105.01626
Company Release Point Description:	Base Elevation (ft):	4553
	Stack Height (ft):	24
LP Oil & Water Tank Flare	Stack Diameter (ft):	0.25
1PH 1-4 Oil Tank Vents	Exit Gas Velocity (ft/s):	1.46
1PH 1-2 Water Tank Vents	Exit Gas Temp (F):	1850
	Exit Gas Flow Rate (acfm):	4.3
Company Release Point ID:	Release Point Type:	
	Release Point Latitude:	
	Release Point Longitude:	
Company Release Point Description:	Base Elevation (ft):	
	Stack Height (ft):	
	Stack Diameter (ft):	
	Exit Gas Velocity (ft/s):	
	Exit Gas Temp (F):	
	Exit Gas Flow Rate (acfm):	
Company Release Point ID:	Release Point Type:	
	Release Point Latitude:	
	Release Point Longitude:	
Company Release Point Description:	Base Elevation (ft):	
•	Stack Height (ft):	
	Stack Diameter (ft):	
	Exit Gas Velocity (ft/s):	
	Exit Gas Temp (F):	
	Exit Gas Flow Rate (acfm):	

Complete the table below for each fugitive (area, volume, line) release point. List each individual release point on a separate line.

Fugit	ive Release Point Information
Company Release Point ID:	Release Point Latitude:  Release Point Longitude:  Release Height (ft):
Company Release Point Description:	
Company Release Point ID:	Release Point Latitude: Release Point Longitude: Release Height (ft):
Company Release Point Description:	
Company Release Point ID:	Release Point Latitude: Release Point Longitude: Release Height (ft):
Company Release Point Description:	
Company Release Point ID:	Release Point Latitude:  Release Point Longitude:  Release Height (ft):
Company Release Point Description:	





### AMERICAN MOBILE RESEARCH, INC.

P.O. BOX 2909 CASPER, WYOMING 82602 (307) 235-4590 PHONE (307) 265-4489 FAX

### **EXTENDED HYDROCARBON (GLYCALC) LIQUID STUDY**

**CERTIFICATE OF ANALYSIS** 

Company RKI EXPLORATION AND PRODUCTION  Lab Number CR-14390  Date Sampled 6-6-2014	Study Number  Date Tested	
Sample Identification CROW UNIT 37-69-30-1TH PRESS TEAPOT FORMATION	SURIZED CRUDE OIL	
Sample Location DOUGLAS, WYOMING. Sample Pressure 85 PSIG Type Sample SPOT Test Method GPA 2186	Sample Temperature County Sampling Method	CONVERSE

Components	Mole %	Weight %	Liq. Vol. %
Hydrogen Sulfide	0.000	0.000	0.000
Oxygen	0.000	0.000	0.000
Carbon Dioxide	0.064	0.017	0.016
Nitrogen	0.013	0.002	0.002
Methane	0.632	0.061	0.156
Ethane	0.143	0.026	0.056
Propane	0.876	0.231	0.352
iso-Butane	0.967	0.337	0.462
n-Butane	2.580	0.898	1.186
iso-Pentane	1.432	0.619	0.764
n-Pentane	1.845	0.797	0.976
Hexanes	1.668	0.861	1.001
Heptanes	6.421	3.853	4.321
Octanes	16.570	11.335	12.382
Nonanes	11.738	9.016	9.635
Decanes+	51.087	69.625	66.402
Benzene	0.124	0.058	0.051
Toluene	0.462	0.255	0.226
Ethylbenzene	0.139	0.088	0.078
Xylenes	1.659	1.055	0.940
n-Hexane	1.278	0.660	0.767
2,2,4-Trimethylpentane	0.302	0.207	0.229
Totals	100.000	100.000	100.000

### ADDITIONAL BETX DATA

Components	Mole %	Weight %	Liq. Vol. %	
2-Methylpentane	1.193	0.616	0.715	
3-Methylpentane	0.475	0.245	0.285	
n-Hexane	1.278	0.660	0.767	
2,2,4-Trimethylpentane	0.302	0.207	0.229	
Benzene	0.124	0.058	0.051	
Toluene	0.462	0.255	0.226	
Ethylbenzene	0.139	0.088	0.078	
m-Xylene	0.249	0.158	0.141	
p-Xylene	0.995	0.633	0.564	
o-Xylene	0.415	0.264	0.235	
API GRAVITY AT 60/60	F, calculated			51.8
		ed		0.77181
		ANES+ (C10+) FRACTION, ca		0.80927
				166.977
		ECANES+ (C10+) FRACTION		
		SIA, calculated		37.421
		d UID, as Ideal Gas, calculated		
		A, calculated		
		A, calculated		6.435
LDG / G/(LLG) ( G) ElQC	, oaloulatou			0.733

NOTATION: ALL CALCULATIONS PERFORMED USING PHYSICAL CONSTANTS FROM GPA 2145-09, THE TABLES OF PHYSICAL CONSTANTS FOR HYDROCARBONS AND OTHER COMPOUNDS OF INTEREST TO THE NATURAL GAS INDUSTRY.

James A. Kane, President
American Mobile Research, Inc.



### AMERICAN MOBILE RESEARCH, INC.

P.O. BOX 2909 CASPER, WYOMING 82602

Company...... RKI EXPLORATION AND PRODUCTION

(307) 235-4590 PHONE (307) 265-4489 FAX

### EXTENDED HYDROCARBON LIQUID STUDIES

### CERTIFICATE OF ANALYSIS

Lab Number         CR-14390           Date Sampled         6-6-2014		udy Number CR-3 ate Tested 6-11-2014				
Sample Identification CROW UNIT 37-69-30-1TH FLASHED CRUDE OIL TEAPOT FORMATION						
Sample Location WYOMING	G.					
Sample PressureN/A		ample Temperature N/A				
FlowrateN/A		ountyCONVERSE				
Test MethodVARIOUS	Sa	ample Container 1-QUART BOTTLE				
TEST PERFORMED		RESULTS				
API GRAVITY AT 60/60 F (ASTM	1 D-287), observed	40.6				
SPECIFIC GRAVITY AT 60/60 F	(ASTM D-1657), calculated	0.8222				
REID VAPOR PRESSURE (AST	M D-323), PSIG AT 100 F, observed	6.8				
TOTAL SULFUR CONTENT (A	STM D-5453), PPMW					
TRUE VAPOR PRESSURE (AST	'M 2889), PSIA AT 100 F, observed	N/A				
BASIC SEDIMENT AND WATE	R CONTENT (BSW), % BY VOLUME	N/A				
COPPER STRIP CORROSION (	ASTM D-130), 1 HOUR AT 100 F, obser	erved N/A				
FREE WATER, observed		N/A				
NOTATION AND TESTING BROWLDS	ON A DOME WAS DEDECTIVED IN ACCORDAN	NOT TO METHODOLOGY				

 ${\tt NOTATION: ALL\ TESTING\ PROVIDED\ ABOVE\ WAS\ PERFORMED\ IN\ ACCORDANCE\ TO\ METHODOLOGY}\\ OUTLINED\ BY\ THE\ AMERICAN\ SOCIETY\ FOR\ TESTING\ AND\ MATERIALS\ (ASTM).}$ 

James A. Kane, President

American Mobile Research, Inc.



### AMERICAN MOBILE RESEARCH, INC.

P.O. BOX 2909 CASPER, WYOMING 82602 (307) 235-4590 PHONE (307) 265-4489 FAX

### **EXTENDED HYDROCARBON GAS (GLYCALC) STUDY**

**CERTIFICATE OF ANALYSIS** 

Company RKI EXPLORATION AND PRODUCTION Lab Number CR-14390 Date Sampled 6-6-2014	Study Number CR-1 Date Tested 6-9-2014
Sample Identification CROW UNIT 37-69-30-1TH TEAPOT FORMATION	
Sample Location DOUGLAS, WYOMING.	
Sample Pressure 24 PSIG	Sample Temperature 77 F
Type Sample SPOT	County CONVERSE
Test Method GPA-2286	Moisture Content N/A

Components	Mole %	Weight %	Liq. Vol. %
Carbon Dioxide	1.143	2.078	0.992
Hydrogen Sulfide	0.000	0.000	0.000
Nitrogen	2.707	3.133	1.514
Methane	74.806	49.583	64.487
Ethane	3.814	4.738	5.187
Propane	8.215	14.967	11.509
iso-Butane	2.091	5.021	3.479
n-Butane	3.723	8.940	5.968
iso-Pentane	1.092	3.255	2.031
n-Pentane	1.098	3.273	2.024
Cyclopentane	0.057	0.165	0.086
n-Hexane	0.269	0.958	0.562
Cyclohexane	0.076	0.264	0.131
Other Hexanes	0.338	1.203	0.707
Heptanes	0.323	1.337	0.758
Methylcyclohexane	0.089	0.361	0.182
2,2,4-Trimethylpentane	0.036	0.170	0.095
Benzene	0.006	0.019	0.009
Toluene	0.014	0.053	0.024
Ethylbenzene	0.006	0.026	0.012
Xylenes	0.015	0.066	0.030
C8+ Heavies	0.082	0.387	0.214
Totals	100.000	100.000	100.000

### ADDITIONAL BETX DATA

Components	Mole %	Weight %Lio	q. Vol. %
Cyclopentane	0.057	0.165	0.086
Cyclohexane	0.076	0.264	0.131
2-Methylpentane	0.242	0.860	0.505
3-Methylpentane	0.096	0.343	0.201
n-Hexane	0.269	0.958	0.562
Methylcyclohexane	0.089	0.361	0.182
2,2,4-Trimethylpentane	0.036	0.170	0.095
Benzene	0.006	0.019	0.009
Toluene	0.014	0.053	0.024
Ethylbenzene	0.006	0.026	0.012
m-Xylene	0.002	0.010	0.004
p-Xylene	0.009	0.039	0.018
o-Xylene	0.004	0.016	0.007
SPECIFIC CRAVITY AT	60/60 E. calculat	rad.	0.835
SPECIFIC GRAVITY AT 60/60 F, calculated			
CALCULATED BTU / REAL CF AT 14.73 PSIA, dry basis			
CALCULATED BTU / REAL CF AT 14.73 PSIA, wet basis			
AVERAGE MOLECULAR WEIGHT.			
MOLAR MASS RATIO			
RELATIVE DENSITY (G x Z (Air) / Z), calculated			
IDEAL GROSS HEATING VALUE, BTU / IDEAL CF AT 14.696 PSIA, calculated			
COMPRESSIBILITY FACTOR (Z)			
PROPANE GPM			
BUTANE GPM			
GASOLINE GPM (PENTANE AND HEAVIER)			

NOTATION: ALL CALCULATIONS PERFORMED USING PHYSICAL CONSTANTS FROM GPA 2145-09, THE TABLES OF PHYSICAL CONSTANTS FOR HYDROCARBONS AND OTHER COMPOUNDS OF INTEREST TO THE NATURAL GAS INDUSTRY.

James A. Kane, President American Mobile Research, Inc.

RKI Exploration & Production, LLC
Split Hill 37-68-27 PAD 1TH (Teapot Formation)
sw sw 27-37N-68W
Converse County, Wyoming

## Gas Analyis from AMR Analysis (6/9/2014)

94.79 40.45 1.29

Wt % HC: Wt % VOCs: Wt % HAPs:

RKI Exploration & Production, LLC Split Hill 37-68-27 PAD (Teapot Formation) sw sw 27-37N-68W Converse County, Wyoming

# Oil Tank Flash Gas Analyis from E&P TANKS 2.0 Run (07/13/2015)

(6) (7) <u>VOC MW</u> HAP MW	7 2.0244 2.0244 3.7556 8 0.9348 0.8788 0.2627 0.3685 0.3212 0.0031 0.00130 0.0130 0.0150 0.0156 0.0016 0.0016 0.0016 0.00155 0.01545 0.0155	
(5) HC MW	10.9197 1.3260 3.6550 2.0244 3.7556 0.9348 0.8788 0.3685 0.3685 0.0031 0.0016 0.0150 0.0154 0.0154	
(4) Gas MW	- 1.4588 0.6154 10.9197 1.3260 3.6550 2.0244 3.7556 0.9348 0.8788 0.2627 0.3685 0.3212 0.0001 0.0015 0.0150 0.0155	
(3) Comp MW	34.08 32.00 44.01 28.01 16.04 30.07 44.10 58.12 72.15 72.15 72.15 86.18 100.20 114.23 78.11 92.14 106.17 86.18	
(2) mol fraction	. 0.0331 0.0230 0.6807 0.0441 0.0348 0.0348 0.0446 0.0122 0.0037 0.0037 0.0002 0.00000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.0000 0.00000 0.000	
(1) mol <u>%</u>	- 3.3146 2.1969 68.0696 4.4100 8.2887 3.4831 6.4615 1.2957 1.2181 0.3049 0.3678 0.0648 0.00167 0.0167 0.0163 0.0156	
Component	H2S O2 C02 N2 C1 C2 C3 i-C4 n-C4 i-C5 C6 C7 C8 C9 C10+ Benzene Toluene E-Benzene Xylenes n-C6 224 Trimethylpentane Totals	

92.27 46.61 0.81

Wt % HC: Wt % VOCs: Wt % HAPs: